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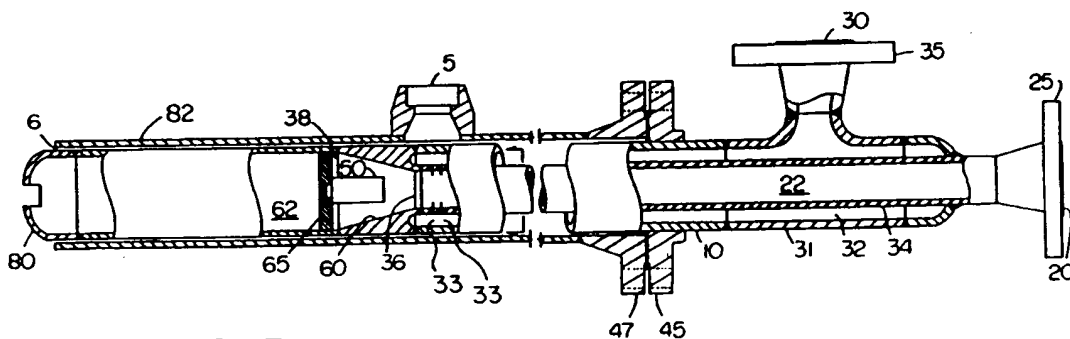
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(54) **Heavy hydrocarbon feed atomization.**

(57) A nozzle, and FCC process using the nozzle for atomizing heavy feed to a riser reactor, are disclosed. A liquid feed stream is atomized by radial out-to-in impingement of atomizing vapour, discharged onto an impingement plug in an annular expansion region, then sprayed through an outlet. Baffles at the expansion region outlet, and an orifice outlet improve feed atomization and feed/FCC catalyst contact in a riser reactor. The nozzle may be used to distribute liquid over other reactor beds, or to add liquid to distillation columns.

**FIG. 5****EP 0 546 739 A2**

This invention relates to heavy hydrocarbon feed atomization. More particularly the invention relates to a process for atomizing liquid feed to refinery process, such as distillation columns or an FCC riser reactor and to an apparatus for atomizing liquids.

Refiners have long known that feed atomization in the base of FCC riser reactors is a problem. It is difficult to contact many tons per hour of hot, regenerated cracking catalyst with large volumes of heavy oil feed, and ensure complete vaporization of the feed in the base of the riser reactor. Part of the problem is use of heavier feeds in FCC units. Many FCC's now process significant amounts, on the order of 5 - 20 % of resid or non-distillable material. These materials are almost impossible to vaporize in fractionators, so vaporizing them in less than a second or so in an FCC riser reactor is a formidable task.

Part of the problem is that feed nozzles which were perfectly satisfactory for adding a readily vaporizable feed, such as a gas oil, are no longer adequate for heavier feeds. The problems are twofold: the heavier feeds are harder to vaporize because of their high boiling points, and the heavy feeds are harder to atomize because of their high viscosity even at the high temperatures existing in FCC riser reactors.

Efforts of refiners to cope with heavier feeds, or improve the vaporization of lighter ones, will be briefly reviewed.

Some of the efforts at improving regenerated catalyst/feed contacting were on the catalyst side, i.e., the use of lift gas to smoothly lift catalyst up into the riser. Other approaches assumed that catalyst distribution will be poor and forced oil distribution (via multiple nozzles) to be equally poor.

Increased steam addition is common practice for dealing with heavier feeds. Increased atomization steam usually leads to increased pressure drop across the existing feed nozzles, and increased sour water production. Although some improvement in feed dispersion is usually achieved, the problems of increased sour water production, and limits on pressure at which feed can be delivered to the nozzles inlets, limit the improvement from merely increasing steam rate.

In action to focusing on catalyst/oil distribution and making existing nozzles work better with more steam, refiners considered other nozzle designs. Some very effective nozzle designs were developed but they required unusually high pressure drops across the nozzle for effective operation. Refiners like to operate the feed nozzles at as low a pressure as possible, both to save on capital equipment and operating costs. Many units are limited in the feed pressure, and major capital improvements are needed to use high pressure drop nozzles. Development of high pressure liquid streams also consumes a considerable amount of energy.

A good overview of developments in nozzles is presented in Fluid Catalytic Cracking Report: 50 Years of Catalytic Cracking; A. A. Avidan et al, Oil & Gas Journal, Jan 8, 1990, at page 50. Open pipe or slotted, impact, spiral and critical venturi nozzles have all been tried.

The open pipe or slotted nozzle gives coarse irregular droplet sizes and is not ideally suitable for injecting heavy feeds into an FCC riser reactor.

Critical venturi nozzles, where an oil and steam mixture is passed through a critically sized venturi section into a larger, intermediate chamber and are discharged through a restricted nozzle can achieve very small droplet sizes. These droplets can be completely vaporized in less time than the droplets produced by spiral nozzles, but such nozzles require high liquid pressure drops, and develop a narrow spray pattern.

A hybrid approach, use of high velocity steam (1000 to 1800 ft/sec {305 to 549 m/s}) to atomize a low velocity oil stream (20 to 50 ft/sec {6 to 15 m/s}) was disclosed in US-A-3654140. The high velocity steam imparts energy to the low velocity liquid. Fig. 2 of US-A-3654140 shows oil discharged as a cone of liquid which is broken into droplets by a high velocity steam stream enveloping the cone. The design was an improvement over the nozzle shown in US-A-3152065, an earlier nozzle developed wherein liquid passed through an annular region about a central steam pipe to contact an expanding steam stream upstream of a restricted opening. Imparting a centrifugal component to the liquid stream probably threw the liquid to the sides of the nozzle, and may have impaired atomization. The liquid went out as a cone and was not impinged by the high velocity steam stream in the central region of the nozzle.

Although there are myriad nozzle designs, many of which are unique and hard to classify, they can be more or less arbitrarily classified as relying on one or more of the following mechanisms for drop formation.

Restriction/Expansion is the most widely used form of FCC feed nozzle. A mixture of 1-5 wt % atomizing steam and the heavy, preheated feed, pass through a slot or circular orifice to form a spray.

Mixing/Expansion involves use of swirl vanes followed by an orifice.

Shearing atomizes liquid by peeling off a thin sheet of the nozzle feed stream which spontaneously breaks up into small droplets. Spiral FCC feed nozzles are examples.

Gas jet nozzles pass an atomizing gas stream through multiple orifices to strike a liquid stream. The Lechler nozzle is a good example of this type of nozzle.

Impingement nozzles atomize by the high velocity impact of a liquid on a solid surface. The Snowjet nozzle is of this type.

Although it might seem possible to simply stack these types of nozzles in series, and thereby improve atomization, this is not possible in practice. Additional stages may or may not improve atomization, but will always increase pressure drop and this alone will usually prevent simple stacking of these unit operations. Many attempts to improve nozzle performance, as by stacking atomizing devices, degrade performance. The addition of swirl vanes to a slotted orifice nozzle has been tried, but this was found to make the distribution worse.

In FCC units, the nozzles must also be robust and reliable, as run lengths of one or two years or more are common. FCC units have additional constraints. The hydrocarbon feeds are supplied at a certain pressure, usually around 50 - 200 psig (446 - 1480 KPa). Because of the large size of these streams, and the cost of energy needed to pump the feed to higher pressures, and site constraints which frequently prevent easy addition of high pressure pumps, it is very important to have a nozzle which will work well with low oil pressures.

Medium or high pressure steam is usually readily available, and is a preferred atomization medium, but refiners usually want to minimize its use. Medium or high pressure steam is a valuable commodity in a refinery, and its use fills much of the FCC riser and downstream processing equipment with an inert material. Refiners are also reluctant to use too much steam, or to have too high an exit velocity from the nozzle, because of catalyst attrition, and riser erosion concerns.

An additional constraint is that the material exiting the nozzle should contact as much of the catalyst flowing by the nozzle as possible, without carrying through the catalyst to a side portion of the riser.

It is also beneficial if the nozzles used, whether vertical or side mounted, are relatively small, so that flow of hot catalyst up the riser is not disrupted.

According to one aspect of the present invention, there is provided an atomizing nozzle comprising: an initial atomization section wherein atomizing gas is charged, in radial out-to-in flow, into a flowing stream containing liquid hydrocarbon, to partially atomize said liquid feed stream and produce a partially atomized jet having a diameter and cross sectional area and having a less atomized core region and a more atomized peripheral region;

an impingement section contiguous with and downstream of said initial atomization section, and having a diameter no greater than the diameter of said initial atomization section;

an annular expansion region about said impingement section, said expansion region having a cross sectional area at least as large as said partially atomized jet and connective with a nozzle barrel having a cross sectional area at least 1.5 times as large as the cross sectional area of said partially atomized jet; and

a nozzle outlet having a cross sectional area smaller than the cross sectional area of said nozzle barrel at an end of said nozzle barrel.

Preferably, said initial atomization section comprises a length of feed pipe having an upstream end connective with a source of liquid feed, a downstream end with an unobstructed or open outlet and plurality of atomizing gas injection holes drilled through said feed pipe and radially distributed about said pipe and within one feed pipe diameter of said outlet, and an atomizing gas distribution section having an inlet for atomizing gas and an outlet encompassing said plurality of atomizing gas injection holes.

Desirably said impingement section comprises a cylindrical plug having an upstream end and a downstream end which is axially aligned with said initial atomization section. The upstream end of said plug preferably has a conical end portion with an angle no greater than 20°.

The plug can be supported at the downstream end thereof, and the support preferably comprises an X or cross-shaped support means, and wherein the support means has a cross sectional area, perpendicular to fluid flow, of 40 to 60 % of the area available for fluid flow immediately upstream of the support means, and said support means splits fluid flowing therethrough into several streams. The downstream support for the cylindrical plug is adapted to split the fluid flowing therethrough into four pie-shaped streams. An outlet of said annular expansion region may comprises said downstream support for said cylindrical plug.

The annular expansion region is desirably axially aligned with said nozzle barrel and has an outlet contiguous with said nozzle barrel. The annular expansion region preferably comprises a truncated conical section having an inlet contiguous with said atomization section, and the nozzle barrel is preferably cylindrical.

The nozzle outlet may comprises a dome or 180° hemi-spherical cap with a rectangular slot opening. Preferably the slot opening is less than 180° and produces a spray angle of 35 to 120°, more preferably 40 to 90°.

The annular expansion region may have a cross sectional area at least as large as the cross sectional area of said partially atomized jet and said expansion region connects with a nozzle barrel having a cross

sectional area at least twice as large as said cross sectional area of said partially atomized jet.

In one construction the nozzle outlet comprises a slot or notch adapted to develop a flat, fan shaped spray, and said nozzle barrel has a length and a diameter, and the ratio of the length to diameter ranges from 3:1 to 15:1, preferably from 3:1 to 6:1, and more preferably 4:1. The nozzle outlet ideally comprises a single rectangular notch outlet.

In said annular expansion region, the nozzle barrel preferably has a cross sectional area 1.5 to 6 times as large as the cross sectional area of said partially atomized jet. more preferably the nozzle barrel has a cross sectional area four times as large as the cross sectional area of said partially atomized jet.

According to another aspect of the invention there is provided a fluidized catalytic cracking process wherein a heavy feed is catalytically cracked in a riser cracking reactor means to produce cracked products and spent catalyst, spent catalyst is stripped in a stripping means and regenerated in a catalyst regeneration means to produce hot regenerated catalyst which is recycled to said riser reactor, wherein at least one multi-stage atomizing feed nozzle as described above is used to inject feed in a base portion of said riser reactor. Preferably a plurality of said nozzles are used. According to another aspect of the invention there is provided a process for adding a normally liquid hydrocarbon feed to a vapour/liquid fractionation means comprising adding said liquid feed and atomizing steam into a vapour phase region of said fractionation means using the nozzle described above.

According to another aspect of the invention there is provided a hydroconversion process for catalytic hydroconversion of a normally liquid hydrocarbon stream by adding hydrogen containing gas and liquid hydrocarbon to a vapour fill region above a fixed bed of catalyst and passing said liquid and hydrogen down through said fixed bed of catalyst at catalytic hydroconversion conditions to produce a hydroconverted product said normally liquid hydrocarbon feed, and at least a portion of said hydrogen containing gas, being added to said vapour full region above said fixed bed feed using the nozzle described above.

The nozzle according to the invention combines several different mechanisms for droplet formation, and achieves efficient atomization, with relatively low amounts of atomizing fluid, without requiring inordinately high oil feed pressures, or impinging on the wall of the riser reactor. The nozzle does not exhibit slugging characteristics, and can be mounted either vertically or at a slant, which permits its use in riser reactors having side mounted nozzles. The design is both robust and compact, and catalyst flows readily around it.

Reference is now made to the accompanying drawings, in which:

- Fig 1 and Fig 2 (prior art) show different views of a 180° slotted cap nozzle outlet;
- Figs. 3 and 4 show views of a shortened slot nozzle outlet;
- Figure 5 shows a cross sectional view of a preferred nozzle according to the invention, with an initial atomizing section, low pressure drop plug and baffle (which also serves as an expansion section) and a shortened slot nozzle outlet;
- Figures 6 and 7 show different views of the low pressure drop plug and baffle;
- Figure 8 is a cross sectional view of the initial atomizing section;
- Figure 9 is a cross sectional view of an FCC riser reactor with a plurality of feed nozzles; and
- Figure 10 is a cross sectional view of the expansion plug, showing a preferred anchoring means.

The state of the art in regard to FCC feed nozzles, or at least feed nozzle outlets, is represented by Figs 1 and 2. The end of a nozzle 80', with notch or slot 85', sprays liquid feed into FCC risers. The feed upstream of the nozzle 80' is an atomized mixture of steam, or other atomizing fluid, and liquid hydrocarbon feed, usually with a minor amount of vaporized hydrocarbon feed. The slot orifice 85' is usually a cut out or ground out portion of the nozzle 80'. Typically the slot orifice has a 180° opening, and has a width or open portion equivalent to 15 - 50% of the diameter of the pipe or end cap 80' containing the slot orifice.

In these orifice nozzles, or those shown in the Oil and Gas Journal report referred to above, oil and steam are injected into a pipe, the end of which terminates in a reduced diameter orifice. The nozzle atomizes or disperses the oil by imparting a high velocity to the oil and atomizing steam. Poor results are obtained, especially with heavy, difficult to vaporize feeds. These nozzles were satisfactory when processing readily distillable feeds, such as gas oils, but their deficiencies become more evident with feeds containing more than about 5 wt % non-distillable material. The problem is that much of the liquid feed is poorly atomized. The large liquid droplets can take a long time to vaporize, or may not vaporize at all and form coke. In some units the feed is not vaporized until after the catalyst is significantly deactivated.

The FCC process and nozzle of the present invention use several mechanisms to form finely atomized droplets of heavy oil. An overview of the three atomization stages or mechanisms of a preferred nozzle follows, with primary reference to Fig 5, and passing reference to other Figs.

Briefly, the nozzle will have an initial atomization section, a low pressure drop impingement and expansion section, and an orifice tip.

The heavy oil or heavy liquid feed is charged via inlet 20 to atomizing chamber 22 of nozzle 10. Flange assembly 45 mates with flange 47 and nozzle shield 82 which extends into the FCC riser reactor.

The oil comes in inlet 20, usually as a liquid phase, and is atomized to a considerable extent as it flows through chamber 22 by the injection of steam transversely into the flowing liquid. Steam is admitted via atomizing fluid inlet 30. Flanges 35 and 25 around inlets 20 and 30, respectively, permit field connection of steam and oil lines.

The steam enters into the annular space 32 between the walls 34 of atomization chamber 22 and the walls 31 of nozzle 10. The steam passes through a plurality of holes 33 preferably drilled at right angles through pipe wall 34.

The heavy oil feed is vigorously mixed, and atomized to a significant extent, as it passes from inlet 20 to outlet 36 of the initial atomization zone. The liquid thus flows axially and the gas passes radially from the annular region 32 surrounding region 22.

Fig 8, which is a section of region 22 taken near the outlet end thereof, shows how steam can flow from the annular steam passageway 32 through holes 33 in pipe 34 to enter region 22 and atomize liquid feed flowing therethrough. Two rows of eight holes each are preferred.

Fig 5 shows the preferred arrangement of steam holes 33, within one or two pipe diameters upstream of the outlet 36 of this section. Preferably the steam holes are within 0.5 inch (1.3 cm) of the outlet 36. If desired, the steam injection holes 33 can be shifted upstream, or supplanted with additional steam injection means, such as slots, tubes, or minor amounts of steam added with the heavy oil feed.

The atomized two phase mixture from outlet 36 is discharged into a low pressure drop impingement and expansion section.

The first step is discharge of the oil/steam mixture directly onto impingement plug 50, which preferably has a cross sectional area no greater than that of the atomizing chamber 22. Ideally, the impingement plug 50 will have a cross sectional area from 30 to 60 % of the cross sectional area of the pipe 34. If pipe 34 is 1.5 inch (3.8cm) Schedule 80 pipe the optimum cross sectional area of plug 50 is around 1 inch (2.5cm). This is large enough to allow for impaction.

Plug 50 should be placed within a low pressure drop expansion region which permits efficient expansion of atomized oil and steam through this portion of the nozzle. The use of a truncated, inverted cone section 60 having an ID approaching or equalling that of the ID of the outlet of region 22 in pipe 34, and an angle of 5 to 30° from centerline, preferably 10 to 25°, and most preferably 15°, will minimize pressure losses due to expansion. More complex geometries, such as those used in venturi meters or carburetors may also be used, but such shapes are harder to fabricate and more expensive. Plug 50 may be somewhat displaced from, or recessed from, the outlet 36 of the initial atomization section, along the direction of liquid flow, by an amount equal to 0.5 inch (1.3cm) or more of the diameter of the outlet 36.

The angle of the inverted cone section 60, and the amount of recess of the impingement plug 50 from outlet 36, should be sufficient to provide a cross sectional area available for fluid flow around plug 50 at least equal to that of the cross sectional area available for fluid flow within pipe 34. Preferably the minimum open area of the pipe around the plug is at least 130 % or more of the cross sectional area of pipe 34. We believe the best spacing is one which will provide about 1.4 times the open area of the feed pipe 34.

Fig 7 shows a cross sectional view of a preferred impingement plug 50. The major purpose of plug 50 is as an impactor, upon which the atomized mixture of oil and steam strikes and further atomization occurs. Preferably the end of the plug is cut at a slight angle, ranging from 2 or 3° to perhaps as much as 15 or 20°, and ideally around 10°. This shallow angle allows for a strong impact of liquid and atomizing fluid against the plug and good atomization, while simultaneously channelling flow evenly around the plug and into the expansion section next to and downstream of the end of plug 50. The plug channels the atomized mixture away from the centre of the pipe into the expansion section.

The expansion section should have an outlet diameter roughly equal to that of the bore of the pipe or tube leading to the nozzle outlet. Preferably the expansion section terminates with a baffle section 65. Preferably the baffle is roughly in the form of a cross or "X", defining four pie shaped openings through which atomized feed passes. These baffles, shown as an interior view in Fig 6, preferably have a spoke width equal to 15 to 35 %, ideally 20 to 30 %, of the diameter of the outlet of the expansion section. A preferred design is the one shown, with a baffle plate having a thickness of 0.5 inch (1.3cm), and each spoke having a width of 0.69 inch (1.8cm), for use within a 3 inch (7.6cm) pipe.

This baffle design provides a good method of distributing droplets across the cross-section of the nozzle barrel, and provides enough metal or other material to support impingement plug 50. An alternative is to use a solid plate, with 2, 3, 4 or more holes drilled in the plate. Use of a solid plate with 4 holes drilled in it will behave hydraulically much like the "X" baffle shown by dotted lines in Fig. 6.

Regardless of the exact shape or configuration of the baffle 65, it is important to have sufficient open area so that there will be only a modest pressure drop across the baffle. Usually providing an open area of at least 25 % of the cross sectional area of the outlet of the expansion section will suffice.

Fig. 10 shows a preferred way of fabricating the plug and baffle assembly, relying on pin 67 to ensure proper placement of the assembly in the nozzle. Field fabrication is greatly simplified, as the unit can not be installed backwards. Field replacement is also easy with such a design.

Baffles 65 promote further mixing of steam and oil, and ensure that the region of the nozzle downstream of the expansion section, and upstream of the nozzle outlet, i.e., the bore of the nozzle outlet, is loaded with an atomized mixture having a uniform droplet size and spray concentration. To this end, spiral mixers, swirl vanes, or baffle sections of varying geometry may be inserted at, or immediately upstream or downstream of the outlet of expansion section, but not necessarily with the same results.

There is a small pressure drop associated with the use of a plug, or plug and baffle, but this pressure drop is efficiently used by the system to atomize the mixture.

The method and apparatus of the present invention can use conventional orifice technology to discharge the atomized mixture into the riser reactor. In general, such orifices work best when the cross sectional area of the orifice is significantly less than the cross sectional area of the snout or barrel just upstream of the orifice. Broad variation in snout:slot areas is possible, but a 3.8:1 ratio gives good results.

The orifice may have additional atomizing means within or just downstream of the orifice tip, such as a spiral nozzle, but these generally will not be needed, and will increase the pressure drop, complexity, and failure rate unduly.

A slot orifice, in the form of a notch or slot 85 is shown in Fig 6. This forms a flat fan spray with an angle less than 180° . This is preferred for FCC use with side or circumferential mount nozzles. When nozzles are vertically mounted, a round orifice outlet is preferred.

The orifice may operate with wedge or deflector means or blocks just upstream of, within, or downstream of the orifice, if desired. These will increase the pressure drop through the nozzle, and the increased atomization efficiency will usually not justify the increased pressure drop. Swirl vanes seem to degrade performance. Thus it is preferred to operate with an orifice outlet consisting essentially of an orifice, preferably a slotted orifice defining a fan shaped spray.

The slotted orifice is preferred for side mounted nozzles, because experiments have shown that such a shape efficiently distributes the atomized mixture into the riser reactor. Although a prior art slot orifice, such as shown in Fig 1 or 2 can be used, it is preferred to use a slot which is shortened away from the tangent line of the cap, as shown in Fig 3 or 4. The slot orifice shown in Fig 3 and 4 will produce a spray angle of approximately $70-80^\circ$, which is a better spray angle for FCC than that produced by a slot orifice cut to the cup tangent line.

Use of such a reduced angle of spray allows the slotted orifice to be placed fairly near the walls of the riser reactor, without eroding the riser wall. Alternatively, the nozzle assembly can be inserted further into the riser reactor, with the increased distance from the riser wall providing some protection from wall erosion.

Fig 9 shows a good way to dispose FCC feed nozzles 10 in the base of an FCC riser reactor 1.

The effectiveness of the feed mixing nozzle of the present invention, was compared to several conventional designs, including an orifice tip nozzle, and an orifice tip nozzle having a spiral outlet.

The experiments were conducted with air/water mixtures, using a standard test procedure which had proved useful for predicting nozzle performance in FCC units. Although FCC units never inject water/air mixtures, by coincidence the flowing properties of these water/air mixtures are similar to those of steam/heavy oil mixtures used in FCC units.

The experiments were conducted in two stages - an initial screening test, followed by more rigorous tests.

The screening tests were run with nozzle exit velocities of 225 and 300 ft/s (69 and 91 m/s), and with dispersion air rates of 1.9 and 4.8 wt%, resulting in four combinations. Observations were qualitative - a video camera, with high shutter speed capability, was used to capture flow patterns and droplet sized more clearly. Tests were performed with the nozzles situated at 30° with respect to horizontal, to simulate the orientation of nozzles in many commercial FCC's with side mounted nozzles. Air was supplied at 100 psig (791KPa), using a large mobile compressor. Centrifugal pumps were used when high liquid flow rates or pressures were needed, with flow rates determined with a turbine or orifice flowmeter. The test procedure used is not critical, because the same test procedure was used for all nozzles.

Standard Commercial Nozzle - A nozzle currently used commercially in FCC units consists of a length of 3 inch (7.6cm) Schedule 40 pipe, with an oil inlet (water inlet) and steam (air) inlet in a "Y" inlet, so that the atomizing fluid was added at a slant, and in the direction of liquid flow. The two fluids flow together for about 3 ft (0.91m) before exiting through a cap with a semi-circular, rectangular slot, similar to that shown in

Fig 1. Both atomization and droplet distribution were poor. Large droplets persisted in the centre and edge regions of the fan shaped, flat spray, while most of the air passed between these large droplet regions. Air and water pressure drops were relatively small. For this nozzle, and most of the others, spray became more uniform and less coarse for the test cases with higher exit velocities. Slugging within the two phase region of the 3 inch (7.6cm) cannon was noticed at the higher flow rates.

Spiral - A commercially available spiral nozzle was also tested. This was mounted on the 3 inch (7.6cm) cannon, with water and air premixed upstream. This nozzle operates by slicing off sheets from the inner cylindrical flow with a spiral cutting plane. This nozzle performed poorly at the 30° test angle since larger droplets predominated at the bottom, with finer droplets at the top. The distribution did improve substantially as the water flow rate increased, but the average droplet size also increased. This nozzle would be most effective when mounted nearly vertically. The air and water pressure drops were low to moderate. The spray contained gaps within the flow since the water remained predominantly in the spiral sheet. The angle of the spray was also moderate, roughly 65°.

Lechler Supersonic - This nozzle has a converging section, with 16 air jets, emerging from 3/16 inch (0.48cm) orifices situated along four circumferential rows, which impinge perpendicularly into a cylindrical core of water. The nozzle then has a diverging section. This nozzle produced good atomization around the outer edge of the spray, but very large droplets persisted in the centre. It may be speculated that this might result from poor air jet penetration into the water, due to low jet velocities. The air jets created a back pressure effect which caused liquid pressure drops to be high for the standard conditions, 22-45 psi (152-310 KPa). Liquid pressure drops changed dramatically with air flow rates. Air pressure drops were low, ranging from 17-28 psi (117-193 KPa). The spray angle produced by the nozzle was very narrow.

SnowJet - This nozzle, manufactured by Spraying Systems Co. feeds air and water into a mixing chamber through fairly small orifices directed toward an impacting cylinder. A 2.5 ft (0.76m) snout, with semi-circular slot, was added by us on the end to create a spray pattern and exit velocity consistent with commercial FCCU requirements. This design achieved good atomization and droplet distribution, but at the cost of very high liquid pressure drop. When flow rates were low coarse droplets began to appear at the edges of the spray. Liquid pressure drops were high, ranging from 33 psi (228 KPa) up to 160 psi (1103 KPa) at the design point, while the air pressure drops were 20-55 psi (138-379 KPa). Two other caps were also tested, these were smaller ones used in snow making. They had smaller exit orifices, which increased pressure drop and exit velocity, but still achieved good atomization. These small exit orifice nozzles had too small a spray pattern, and too high an exit velocity to have much practical utility as FCC feed nozzles.

Modifications - Several modifications were made to some of the standard designs, some of which degraded performance, or resulted in unacceptable increases in pressure drop.

Adding swirl vanes upstream of the standard commercial nozzle discussed above produced a highly distorted "s" shaped spray, with coarse droplets at the edges.

When using a slot orifice outlet on a commercially available nozzle with internal swirl vanes, the swirling forced large droplets of water toward the edges, while the air bypassed through the middle.

Invention - Good atomization could be achieved using a nozzle with three sections or stages - an initial atomizing section, an impingement plug with low pressure drop expansion section, and an orifice outlet. All parts of the nozzle work together to achieve the desired result. Some conventional nozzle technology can be used in some parts of the nozzle, e.g., an initial atomizing section, or an orifice outlet, similar to that of some prior art nozzles, may be used, with some degradation in performance. Each section or stage will be reviewed in more detail below, along with some of the experimental work that went into devising each section.

Atomizing of feed is an essential first stage in the nozzle. The atomizing section bears some resemblance to the Lechler Supersonic nozzle, but it is not the same. The following differences can be noted. Our design does not require a gradually converging section, but can simply use a length of straight pipe. Rather than add atomizing vapour at four locations (four rings of holes), the atomizing vapour is added via just two locations (two rings). The air holes were sized to utilize fully the pressure drops available on the gas side.

The Lechler Supersonic, and similar types of nozzles, work well around the edges, but have a core problem, that is large droplets tend to persist in the centre of the spray. Going to higher gas rates improves atomization, but can cause a dramatic change in liquid pressure drop.

The preferred design according to the invention, which uses two rows or rings of holes, makes excellent use of all the pressure energy available in the atomizing gas.

The injection of at least one stage of atomizing vapour into a core of liquid via a plurality of radially distributed orifices works well. One ring of four orifices, located within one pipe diameter of the outlet of this section, is probably the minimum configuration, but use of two rows, each with eight orifices is believed

optimum.

The impingement plug, with low pressure drop expansion section, is an important part of the invention. At its simplest it need only consist of a single impingement plug having a cross-sectional area, as measured in the direction of flow ranging from 25 to 150 %, and preferably from 30 to 60 %, and most preferably about 40 to 55 % of the upstream section or feed pipe.

It is especially beneficial if the impingement plug has a cut or ground surface, deflecting flow around the impingement plug with a very shallow cut, not more than 20°, and preferably about 10°. The plug acts as an impactor, upon which the feed strikes and further atomization occurs. The shallow cut, at the end of the plug, channels flow evenly into an annular opening around the plug. Fig 7 shows a preferred impingement plug 50 with ground end.

The open area, or annular area around the plug should be at least as large as the open area of the feed pipe. The optimum open area, for the cut plug tested, is believed to be around 1.4 times the open area of the feed pipe. The relatively large open area, and the deflection action of the impingement pin, provide further atomization, especially of the large droplets that may remain in the central flow regions of the feed pipe. Preferably the annular area is defined at least in part by an expansion area, such as area 60, in which the nozzle ID makes the transition from the relatively narrow atomizing region 22 to the much larger region 62 upstream of the nozzle outlet.

Preferably there is a 5° to 30°, and most preferably a 10° to 20° angle, overall as measured from the centerline, expansion area from the oil feed pipe to the large nozzle pipe. This shallow angle minimises pressure losses due to expansion, which allows available pressure to be used in atomization of feedstock, rather than simply lost due to passing through a sudden expansion of the pipe. The 15° shown in Fig 5 is believed optimum. Use of more exotic shapes, such as a venturi section, may further reduced pressure drop. The preferred plug design has such a low pressure drop associated with it that the higher cost of exotic shapes will not be worth the marginal reduction in pressure drop.

Preferably the expansion region ends with a baffle effective to promote some additional mixing and uniform distribution of droplets in the region upstream of the nozzle outlet. The preferred baffle is a cross shaped means which distributes flow evenly through four large pie-shaped orifices.

The nozzle according to the invention, like many nozzle designs of the prior art, works best with some type of orifice outlet. Although any of the conventional orifice outlets known in the art can be used (such as those shown in the Oil & Gas Journal Article previously discussed), the design works best with a slotted cap outlet such as that shown in Figs 3 and 4. A circular orifice can be used for vertically mounted nozzles, while slots developing a relatively wide fan shaped spray can be used for nozzles mounted circumferentially around the perimeter of an FCC riser.

For use in FCC, the slot open area should be sized to provide an exit velocity of 150 to 450 ft/s (46 to 137 m/s), preferably 200 to 350 ft/s (61 to 107 m/s), and most preferably around 300 ft/s (91 m/s). This is a moderately high exit velocity, which gives the nozzle spray sufficient energy to mix well with the hot catalyst, but not so high as to cause attrition of the catalyst nor carry across the catalyst and impinge on the opposite wall of the riser. Use of a notched or slot outlet, developing a flat, fan shaped spray, avoids formation of a concentrated stream of oil, which might penetrate across the riser.

In the preferred nozzle configuration, all parts function in a complementary fashion. The initial atomizing section does a good job of atomizing most of the liquid feed. The impingement plug does very little to the well atomized oil near the walls of the atomizing section, but is ideally placed to atomize the modest amount of larger droplets remaining in the central regions of the atomizing section, furthest from the wall. Mixing intensity decreases radially inward from the wall of the atomizing section, while the reverse is true in the plug section, where the mixing intensity is highest in the centre.

Additional mixing occurs as the well atomized mixture passes through the four pie shaped openings, and again when the mixture splits to some extent to get through the slot shaped nozzle outlet, which is preferably rotated 45° from the pie shaped openings.

When a notch shaped outlet, generating a flat, fan shaped spray, is used, there is a strong interaction between the baffle and the orifice, which even involves the length of the snout or nozzle barrel holding the orifice. The baffles just downstream of the impingement plug significantly improve performance when a slot outlet is used. There seems to be a significant degradation in performance, in forcing the atomized stream to shift from a generally circular distribution (around the impingement pin) to a flat fan shaped spray. Use of the the baffles, and providing sufficient length of nozzle barrel upstream of the slot orifice to let the pie shaped sprays mix in the nozzle barrel, maintains good atomization. The optimum length of the snout, or length of pipe between the slot orifice and the baffles, is about 4 pipe diameters, but longer or shorter lengths have given acceptable results.

A series of qualitative (screening) and quantitative tests were conducted. A nozzle, very similar to that shown in Fig 5 was used for the tests. The basic nozzle design consisted of an atomizing section (two varieties were tested), an impingement plug with pie shaped opening baffle downstream of the plug, and a length of 3 inch (7.6cm) pipe with a cap with a horizontal slot at the end.

Two atomization sections were tested, one with eight, 5/32 inch (0.4cm) annular air orifices which impinged upon a core of water at 45°, within a region of expansion. This is not shown in the figs. The second, and preferred, design used sixteen, 1/8 inch (0.32cm) annular air orifices situated upstream of the expansion region.

The nozzles tested were oriented vertically downward, to accommodate the analyzing equipment. A droplet size analyser was used to digitise a black and white image of part of the spray which passes through a narrow gap in the line of sight of a video camera. A gap length of 13 mm was used for the experiments. The droplets were back illuminated by a strobing Xenon laser. To ensure statistical significance, data were acquired so that at least 10,000 droplets were analysed. To avoid including erroneously large drops, usually due to splattering, we excluded any single droplet that contributed to more than 10 % of the volume of all droplets. This rarely had to be done, though, since the possibility of this happening was reduced by counting large numbers of droplets during each test. Droplet sizes were calculated as the Sauter mean droplet size, defined as the diameter of a sphere which has the same volume/surface area ratio as that of the total droplet population. Relative droplet sizes were then calculated for each set of tests. Tests were run at various nozzle exit velocities, and with varying amounts of air.

Additional tests were then conducted to determine the effectiveness of the slotted orifice outlet. The same nozzle body was used, for all tests, with both types of atomization sections. In one set of tests, no impingement plug or cap was used. This produced a relatively narrow spray angle of 20° - 30°. In the other series of tests, the 0.8 x 2.9 inch. (2 x 7.4cm) slot in a cap was affixed to the end of the nozzle. The tests are presented in two groupings in Tables I and II, the first being with eight orifices discharging air into the expansion section, and the second being with sixteen orifices, as shown in Fig 5.

A comparison of Tables I and II show that the sixteen orifice nozzle design produces a spray with a significantly smaller dropsize than the eight orifice design. In the sixteen hole design the steam jets impinge upon the feed in a perpendicular direction, which provides for maximum utilisation of the available steam flowrate and pressure.

The impact of several key variables can also be analysed from the data in Table I. The effects of exit velocity and wt% steam are both significant to the performance of the nozzle. As the exit velocity increases at constant wt% steam, the atomization improves. This is also true of wt% steam, as the amount of steam increases relative to the amount of feed (at constant exit velocity), the atomization improves. From 300 to 225 ft/s (91 to 68 m/s) exit velocity and 5 to 2 wt% steam, the performance of the nozzle declines incrementally, but below those values, the decrease in performance becomes more rapid.

Table III studies the impact of the plug and baffle piece and the slotted cap on the atomization performance of the nozzle. Both the eight and sixteen steam orifice tables clearly indicate that the atomization improves with the addition of the plug and baffle and the slotted cap. Comparing the two nozzles, however, shows that the improvement gained by the addition of these pieces is much greater for the eight hole design. This is because the initial atomization generated by the sixteen hole design at the impingement point is very good; there is not as much room for further atomization downstream. The data show that the improvement caused by the plug and baffle and slotted cap for the eight hole design is 30-53%, while the improvement for the sixteen hole design is only 10-15%. What this means is that the sixteen holes do an excellent job of atomizing the feed, and that the plug and cap, while adding some atomization, are mainly responsible for the distribution and formation of the spray pattern.

These tests show that the nozzle according to the invention functions very well using a combination of initial atomization, impaction, and expansion. The nozzle should be widely applicable in refinery and petrochemical processes, and not subject to plugging. The only fine holes in the preferred design are used to admit high pressure steam to the initial atomizing section. The portions of the nozzle wet by hydrocarbon oil (or other liquid feed) are relatively open, i.e., the cross sectional area available for flow around the impingement plug is larger than the cross sectional area available for fluid flow in the initial atomization section.

As applied to hydrotreaters, the use of such a nozzle will significantly improve catalyst use and minimize channelling of feed through the fixed bed of hydrotreating catalyst.

As applied to hydrocrackers, the use of our nozzle will greatly improve the efficiency and the safety of the process, by preventing liquid maldistribution, which can lead to localised areas of high temperature which tend to travel through the hydrocracking bed and get worse. The nozzle can be used for adding liquid feed, and/or liquid quench to hydrocrackers.

The nozzle of the present invention may also be used to add any essentially solids free vapour/liquid phase to any refinery unit operation. The efficiency of packed towers will be greatly improved if the feed is added via an orifice tip nozzle with swirl vanes. In such an application the vapour present in the two phase feed will usually be sufficient to disperse the liquid over the packed column.

TABLE I
Extended Data for the New Nozzles

NEW NOZZLE DESIGN WITH 16 ORIFICES

Run Number	Air wt. %	Exit Velocity ft/s	Exit Density lb/cu.ft	Water Flow gpm	Air Flow scfm	Pressure Drop Liquid	Relative Gas	Droplet size
1	1.0	150	6.89	118	129	29	38.5	3.40
2	1.0	225	6.89	177	194	56	65.3	3.58
3	1.0	300	6.89	235	259	87.6	93.2	2.78
4	2.0	150	3.68	62	137	15.5	32.9	3.13
5	2.0	225	3.68	93	205	31	57.5	1.65
6	2.0	300	3.68	124	273	47	80.3	1.11
7	5.0	150	1.57	26	142	6	35	2.60
8	5.0	225	1.57	39	212	13.1	55.5	1.44
9	5.0	300	1.57	52	283	22	79.1	1.00
10	5.0	350	1.57	60	330	29.1	91.2	1.40

TABLE II
ALTERNATE NOZZLE DESIGN WITH 8 ORIFICES

Run Number	Air wt. %	Exit Velocity ft/s	Exit Density lb/cu.ft	Water Flow gpm	Air Flow scfm	Pressure Drop Liquid	Pressure Drop (psi) Gas	Relative Droplet size
1	2.0	150	3.68	62	137	7.5	37.5	3.22
2	2.0	225	3.68	93	205	18	57	1.71
3	2.0	300	3.68	124	273	28	88.8	1.22
4	5.0	150	1.57	26	142	2	36	3.21
5	5.0	225	1.57	39	212	7	61.5	1.66
6	5.0	300	1.57	52	283	13	90.8	1.27

TABLE III
Extended Data for the New Nozzles

NEW NOZZLE DESIGN

Exit size: 0.8" x 2.9" Spray Angle: 60°-80° (with Plug and Cap)
20°-30° (No Plug and Cap)

New Nozzle Design Options	Exit Velocity ft/sec	Gas wt %	8 Steam Orifices		Relative Droplet size
			Pressure Drop Liquid	Pressure Drop Gas	
No Plug and Cap	225	2	4	62.7	3.61
w/Plug and Cap	225	2	18	57	1.71
No Plug and Cap	300	5	2	88	1.82
w/Plug and Cap	300	5	13	90.8	1.27

New Nozzle Design Options	Exit Velocity ft/sec	Gas wt %	16 Steam Orifices		Droplet size
			Pressure Drop Liquid	Pressure Drop Gas	
No Plug and Cap	225	2	25	55.5	1.95
w/Plug and Cap	225	2	31	57.5	1.65
No Plug and Cap	300	5	18	84.7	1.11
w/Plug and Cap	300	5	22	79.1	1.00

Claims

1. A fluidized catalytic cracking process wherein a heavy feed is catalytically cracked in a riser cracking reactor means to produce cracked products and spent catalyst, spent catalyst is stripped in a stripping

means and regenerated in a catalyst regeneration means to produce hot regenerated catalyst which is recycled to said riser reactor, wherein at least one multi-stage atomizing feed nozzle is used to inject feed in a base portion of said riser reactor, said nozzle comprising:

- 5 an initial atomization section wherein atomizing gas is charged, in radial out-to-in flow, into a flowing stream containing liquid hydrocarbon, to partially atomize said liquid feed stream and produce a partially atomized jet having a diameter and cross sectional area and having a less atomized core region and a more atomized peripheral region;
- an impingement section contiguous with and downstream of said initial atomization section, and having a diameter no greater than the diameter of said initial atomization section;
- 10 an annular expansion region about said impingement section, said expansion region having a cross sectional area at least as large as said partially atomized jet and connective with a nozzle barrel having a cross sectional area at least 1.5 times as large as the cross sectional area of said partially atomized jet; and
- a nozzle outlet having a cross sectional area smaller than the cross sectional area of said nozzle barrel at an end of said nozzle barrel.
- 15 2. A process according to claim 1, wherein a plurality of said nozzles is used.
3. A process according to claim 1 or 2, wherein the impingement section is axially aligned with said initial atomisation section.
4. A process according to claim 1,2, or 3, wherein said initial atomization section comprises a length of feed pipe having an upstream end connective with a source of liquid feed, a downstream end with an
- 20 unobstructed or open outlet and plurality of atomizing gas injection holes drilled through said feed pipe and radially distributed about said pipe and within one feed pipe diameter of said outlet, and an atomizing gas distribution section having an inlet for atomizing gas and an outlet encompassing said plurality of atomizing gas injection holes.
5. A process according to any preceding claim, wherein said impingement section comprises a cylindrical plug having an upstream end and a downstream end which is axially aligned with said initial atomization section.
- 25 6. A process according to claim 5, wherein the upstream end of said plug has a conical end portion with an angle no greater than 20°.
7. A process according to claim 5 or 6, wherein the plug is supported at the downstream end thereof.
- 30 8. A process according to claim 7, wherein the downstream support comprises an X or cross-shaped support means, and wherein the support means has a cross sectional area, perpendicular to fluid flow, of 40 to 60 % of the area available for fluid flow immediately upstream of the support means, and said support means splits fluid flowing therethrough into several streams.
9. A process according to claim 8, wherein said downstream support for the cylindrical plug is adapted to
- 35 split the fluid flowing therethrough into four pie-shaped streams.
10. A process according to any preceding claim, wherein the annular expansion region is axially aligned with said nozzle barrel and has an outlet contiguous with said nozzle barrel.
11. A process according to claim 10, wherein said outlet of said annular expansion region comprises said downstream support for said cylindrical plug.
- 40 12. A process according to claim 10 or 11, wherein the annular expansion region comprises a truncated conical section having an inlet contiguous with said atomization section.
13. A process according to any preceding claim, wherein said nozzle barrel is cylindrical.
14. A process according to any preceding claim, wherein said nozzle outlet comprises an orifice.
15. A process according to claim 14, wherein said nozzle outlet comprises a dome or 180° hemi-spherical
- 45 cap with a rectangular slot opening.
16. A process according to claim 15, wherein the slot opening is less than 180° and produces a spray angle of 35° to 120°, preferably 40 to 90°.
17. A process according to any preceding claim, wherein said annular expansion region about said impingement section has a cross sectional area at least as large as the cross sectional area of said partially
- 50 atomized jet and said expansion region connects with a nozzle barrel having a cross sectional area at least twice as large as said cross sectional area of said partially atomized jet.
18. A process according to any one of claims 1 to 13, wherein said nozzle outlet comprises a slot or notch adapted to develop a flat, fan shaped spray, and said nozzle barrel has a length and a diameter, and the ratio of the length to diameter ranges from 3:1 to 15:1.
- 55 19. A process according to claim 18, wherein said nozzle barrel has a length to diameter ratio of from 3:1 to 6:1, preferably 4:1.
20. A process according to claim 17, 18 or 19 wherein said nozzle outlet comprises a single rectangular notch outlet.

21. A process according to any preceding claim, wherein, in said annular expansion region, the nozzle barrel has a cross sectional area 1.5 to 6 times as large as the cross sectional area of said partially atomized jet.

23. A process according to claim 23, wherein, in said annular expansion region, the nozzle barrel has a cross sectional area four times as large as the cross sectional area of said partially atomized jet.

24. An atomizing nozzle comprising:

an initial atomizer having a generally cylindrical inner surface having an axis, a diameter and a cross sectional area, a first end, a second end, a borehole extending from the first end to the second end, a liquid feed inlet connective with the first end, a plurality of radially distributed atomizing gas inlets drilled through said cylinder and within one diameter of the second end;

an impingement atomizer having an axis which is axially aligned with the axis of said initial atomizer, a first end, a second end, a generally cylindrical plug having a diameter, a plug first end near the atomizing section and a plug second end, said plug being in axially alignment with said initial atomizer and wherein said plug first end is in open fluid communication with said second end of said initial atomizer;

an annular expansion region consisting of a truncated cone having an angle of less than 20° , a first end near the apex thereof connective with said second end of said initial atomizer and a second end connective with a nozzle barrel, and enveloping said impingement atomizer; and

a cylindrical nozzle barrel having an axis and being axially aligned with said initial atomizer, a diameter at least 1.5 times as large as the diameter of said initial atomizer, a first end connective with the second end of said annular expansion region, and a second end connective with an orifice outlet.

24. A nozzle according to claim 23, wherein the diameter of the cylindrical nozzle is at least twice as large as the diameter of said initial atomizer.

25. A process for adding a normally liquid hydrocarbon feed to a vapour/liquid fractionation means comprising adding said liquid feed and atomizing steam into a vapour phase region of said fractionation means using the nozzle of claim 23 or 24.

26. A hydroconversion process for catalytic hydroconversion of a normally liquid hydrocarbon stream by adding hydrogen containing gas and liquid hydrocarbon to a vapour fill region above a fixed bed of catalyst and passing said liquid and hydrogen down through said fixed bed of catalyst at catalytic hydroconversion conditions to produce a hydroconverted product characterized by adding said normally liquid hydrocarbon feed to and at least a portion of said hydrogen containing gas to said vapour full region above said fixed bed feed using the nozzle of claim 23 or 24.

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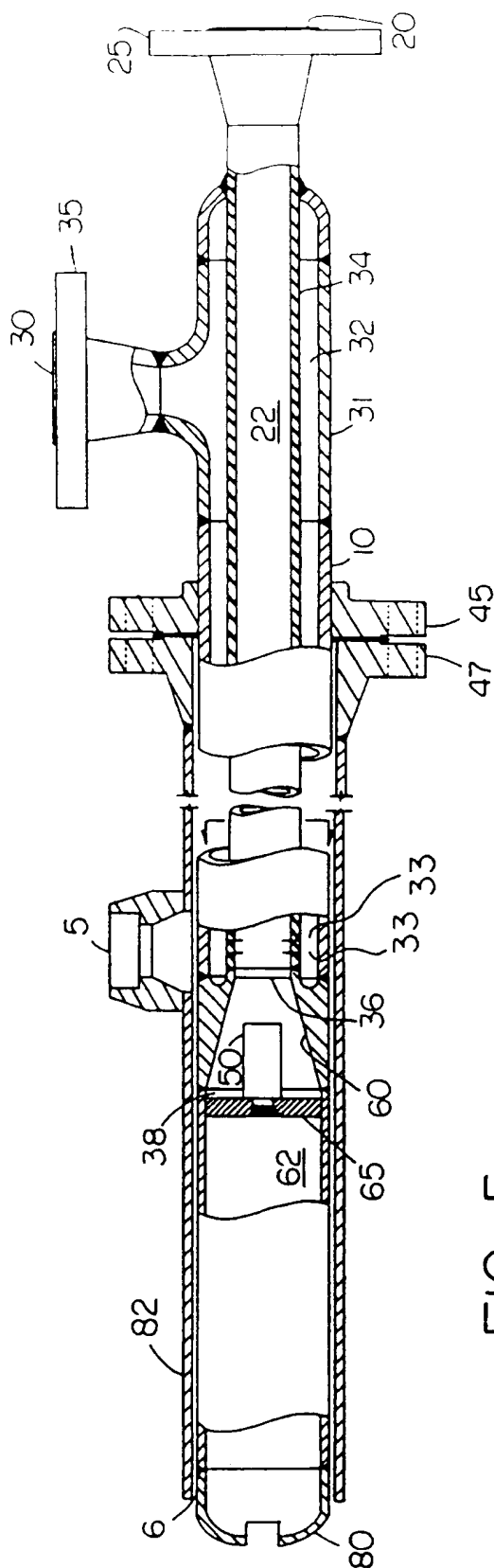
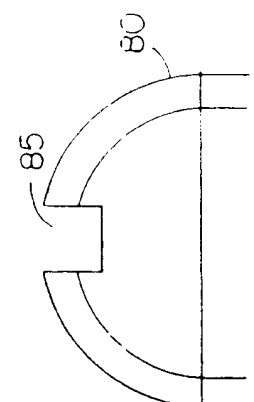
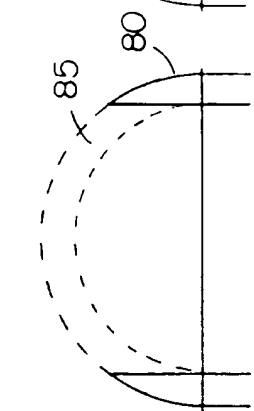
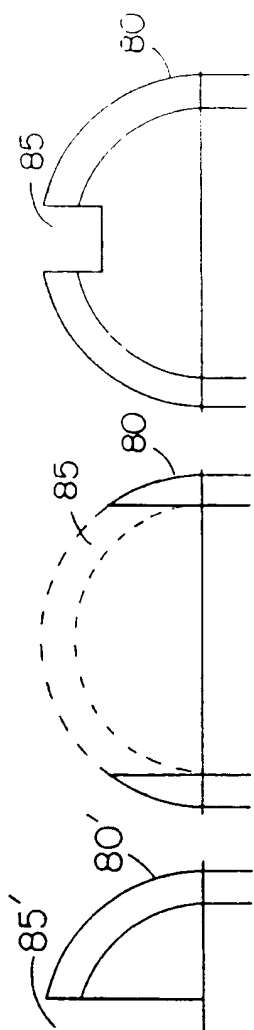
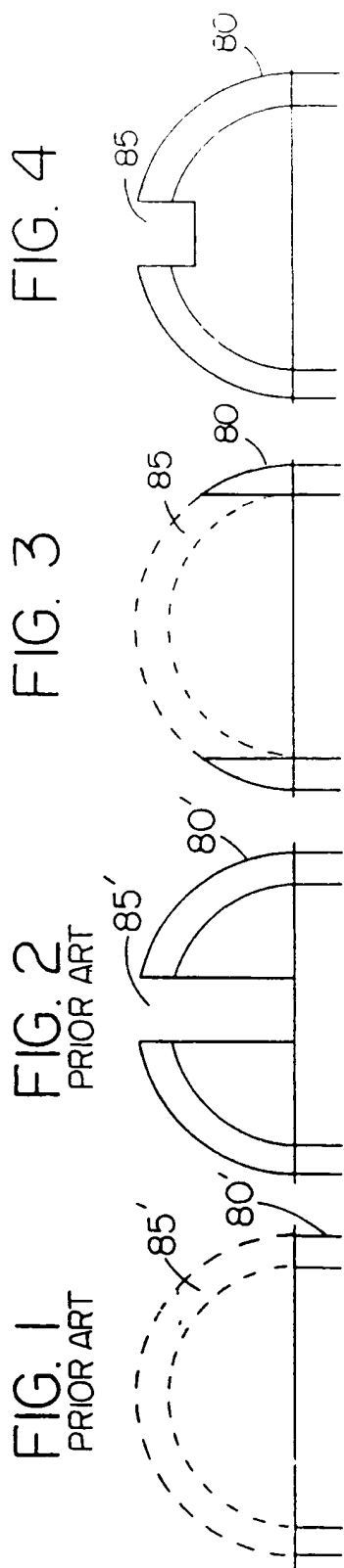


FIG. 6

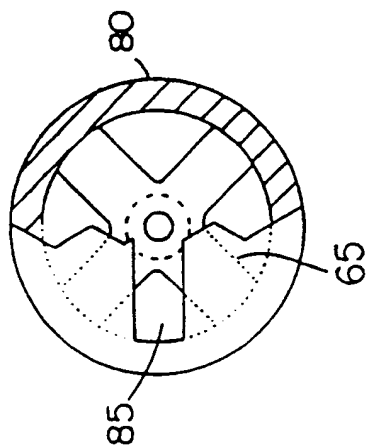


FIG. 7

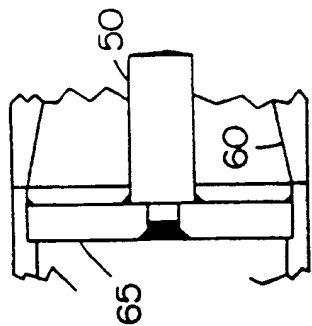


FIG. 8

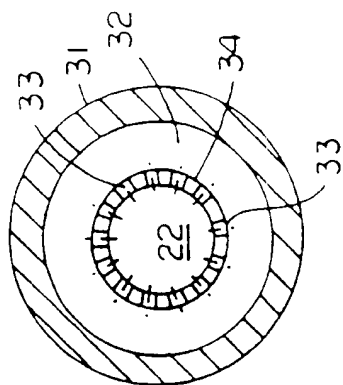


FIG. 9

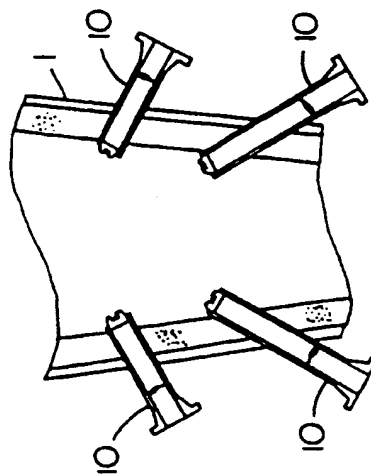
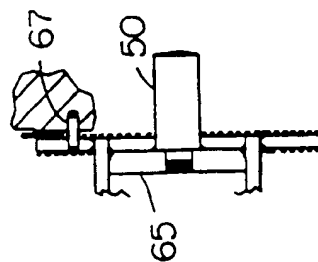


FIG. 10



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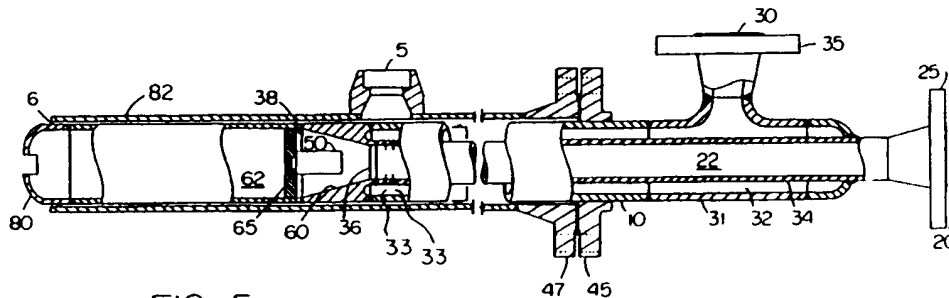
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(54) **Heavy hydrocarbon feed atomization.**

(57) A nozzle, and FCC process using the nozzle for atomizing heavy feed to a riser reactor, are disclosed. A liquid feed stream is atomized by radial out-to-in impingement of atomizing vapour, discharged onto an impingement plug in an annular expansion region, then sprayed through an outlet.

Baffles at the expansion region outlet, and an orifice outlet improve feed atomization and feed/FCC catalyst contact in a riser reactor. The nozzle may be used to distribute liquid over other reactor beds, or to add liquid to distillation columns.

**FIG. 5****EP 0 546 739 A3**



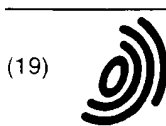
European Patent
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EUROPEAN SEARCH REPORT

Application Number

EP 92 31 0891

DOCUMENTS CONSIDERED TO BE RELEVANT			
Category	Citation of document with indication, where appropriate, of relevant passages	Relevant to claim	CLASSIFICATION OF THE APPLICATION (Int. Cl.5)
A	US-A-4 434 049 (DEAN ET AL) * figure 2 *	1-24	C10G11/18 B01J8/24 C10G49/00 C10G7/00
A	EP-A-0 312 428 (COMPAGNIE DE RAFFINAGE ET DE DISTRIBUTION TOTAL FRANCE) * figures 1,2 *	1-24	
A	EP-A-0 318 185 (CONOCO) * figure 2 *	1-24	
A	WO-A-9 011 337 (IFP) * figures 4,5 *	1-24	
			TECHNICAL FIELDS SEARCHED (Int. Cl.5)
			C10G B01J
The present search report has been drawn up for all claims			
Place of search THE HAGUE		Date of completion of the search 24 JUNE 1993	Examiner MICHIELS P.
CATEGORY OF CITED DOCUMENTS X : particularly relevant if taken alone Y : particularly relevant if combined with another document of the same category A : technological background O : non-written disclosure P : intermediate document T : theory or principle underlying the invention E : earlier patent document, but published on, or after the filing date D : document cited in the application L : document cited for other reasons A : member of the same patent family, corresponding document			



(19)

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(54) Heavy hydrocarbon feed atomization

Atomisierung von schweren Kohlenwasserstoffen

Atomisation d'une charge d'hydrocarbures lourds

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(56) References cited:
**EP-A- 0 312 428 EP-A- 0 318 185
WO-A-90/11337 US-A- 4 434 049**

EP 0 546 739 B1

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Description

This invention relates to heavy hydrocarbon feed atomization. More particularly the invention relates to a process for atomizing liquid feed to refinery process, such as distillation columns or an FCC riser reactor and to an apparatus for atomizing liquids.

Refiners have long known that feed atomization in the base of FCC riser reactors is a problem. It is difficult to contact many tons per hour of hot, regenerated cracking catalyst with large volumes of heavy oil feed, and ensure complete vaporization of the feed in the base of the riser reactor. Part of the problem is use of heavier feeds in FCC units. Many FCCs now process significant amounts, on the order of 5 - 20 % of resid or non-distillable material. These materials are almost impossible to vaporize in fractionators, so vaporizing them in less than a second or so in an FCC riser reactor is a formidable task.

Part of the problem is that feed nozzles which were perfectly satisfactory for adding a readily vaporizable feed, such as a gas oil, are no longer adequate for heavier feeds. The problems are twofold: the heavier feeds are harder to vaporize because of their high boiling points, and the heavy feeds are harder to atomize because of their high viscosity even at the high temperatures existing in FCC riser reactors.

Efforts of refiners to cope with heavier feeds, or improve the vaporization of lighter ones, will be briefly reviewed.

Some of the efforts at improving regenerated catalyst/feed contacting were on the catalyst side, i.e., the use of lift gas to smoothly lift catalyst up into the riser. Other approaches assumed that catalyst distribution will be poor and forced oil distribution (via multiple nozzles) to be equally poor.

Increased steam addition is common practice for dealing with heavier feeds. Increased atomization steam usually leads to increased pressure drop across the existing feed nozzles, and increased sour water production. Although some improvement in feed dispersion is usually achieved, the problems of increased sour water production, and limits on pressure at which feed can be delivered to the nozzle inlets, limit the improvement from merely increasing steam rate.

In addition to focusing on catalyst/oil distribution and making existing nozzles work better with more steam, refiners considered other nozzle designs. Some very effective nozzle designs were developed but they required unusually high pressure drops across the nozzle for effective operation. Refiners like to operate the feed nozzles at as low a pressure as possible, both to save on capital equipment and operating costs. Many units are limited in the feed pressure, and major capital improvements are needed to use high pressure drop nozzles. Development of high pressure liquid streams also consumes a considerable amount of energy.

A good overview of developments in nozzles is presented in Fluid Catalytic Cracking Report: 50 Years of Catalytic Cracking; A. A. Avidan et al, Oil & Gas Journal, Jan 8, 1990, at page 50. Open pipe or slotted, impact, spiral and critical venturi nozzles have all been tried.

The open pipe or slotted nozzle gives coarse irregular droplet sizes and is not ideally suitable for injecting heavy feeds into an FCC riser reactor.

Critical venturi nozzles, where an oil and steam mixture is passed through a critically sized venturi section into a larger, intermediate chamber and are discharged through a restricted nozzle can achieve very small droplet sizes. These droplets can be completely vaporized in less time than the droplets produced by spiral nozzles, but such nozzles require high liquid pressure drops, and develop a narrow spray pattern.

A hybrid approach, use of high velocity steam (1000 to 1800 ft/sec {305 to 549 m/s}) to atomize a low velocity oil stream (20 to 50 ft/sec {6 to 15 m/s}) was disclosed in US-A-3654140. The high velocity steam imparts energy to the low velocity liquid. Fig. 2 of US-A-3654140 shows oil discharged as a cone of liquid which is broken into droplets by a high velocity steam stream enveloping the cone. The design was an improvement over the nozzle shown in US-A-3152065, an earlier nozzle developed wherein liquid passed through an annular region about a central steam pipe to contact an expanding steam stream upstream of a restricted opening. Imparting a centrifugal component to the liquid stream probably threw the liquid to the sides of the nozzle, and may have impaired atomization. The liquid went out as a cone and was not impinged by the high velocity steam stream in the central region of the nozzle.

Although there are myriad nozzle designs, many of which are unique and hard to classify, they can be more or less arbitrarily classified as relying on one or more of the following mechanisms for drop formation.

Restriction/Expansion is the most widely used form of FCC feed nozzle. A mixture of 1-5 wt % atomizing steam and the heavy, preheated feed, pass through a slot or circular orifice to form a spray.

Mixing/Expansion involves use of swirl vanes followed by an orifice.

Shearing atomizes liquid by peeling off a thin sheet of the nozzle feed stream which spontaneously breaks up into small droplets. Spiral FCC feed nozzles are examples.

Gas jet nozzles pass an atomizing gas stream through multiple orifices to strike a liquid stream. The Lechler nozzle is a good example of this type of nozzle.

Impingement nozzles atomize by the high velocity impact of a liquid on a solid surface. The Snowjet nozzle is of this type.

Although it might seem possible to simply stack these types of nozzles in series, and thereby improve atomization,

this is not possible in practice. Additional stages may or may not improve atomization, but will always increase pressure drop and this alone will usually prevent simple stacking of these unit operations. Many attempts to improve nozzle performance, as by stacking atomizing devices, degrade performance. The addition of swirl vanes to a slotted orifice nozzle has been tried, but this was found to make the distribution worse.

In FCC units, the nozzles must also be robust and reliable, as run lengths of one or two years or more are common. FCC units have additional constraints. The hydrocarbon feeds are supplied at a certain pressure, usually around 50 - 200 psig (446 - 1480 KPa). Because of the large size of these streams, and the cost of energy needed to pump the feed to higher pressures, and site constraints which frequently prevent easy addition of high pressure pumps, it is very important to have a nozzle which will work well with low oil pressures.

Medium or high pressure steam is usually readily available, and is a preferred atomization medium, but refiners usually want to minimize its use. Medium or high pressure steam is a valuable commodity in a refinery, and its use fills much of the FCC riser and downstream processing equipment with an inert material. Refiners are also reluctant to use too much steam, or to have too high an exit velocity from the nozzle, because of catalyst attrition, and riser erosion concerns.

An additional constraint is that the material exiting the nozzle should contact as much of the catalyst flowing by the nozzle as possible, without carrying through the catalyst to a side portion of the riser.

It is also beneficial if the nozzles used, whether vertical or side mounted, are relatively small, so that flow of hot catalyst up the riser is not disrupted.

According to one aspect of the present invention, there is provided an atomizing nozzle comprising:

an initial atomization section wherein atomizing gas is charged, in radial out-to-in flow, into a flowing stream containing liquid hydrocarbon, to partially atomize said liquid feed stream and produce a partially atomized jet having a diameter and cross sectional area and having a less atomized core region and a more atomized peripheral region;

an impingement section contiguous with and downstream of said initial atomization section, and having a diameter no greater than 150 % of, preferably no greater than 100 % of, the diameter said initial atomization section;

an annular expansion region about said impingement section, said expansion region having a cross sectional area at least as large as said partially atomized jet and connective with a nozzle barrel having a cross sectional area at least 1.5 times as large as the cross sectional area of said partially atomized jet; and

a nozzle outlet having a cross sectional area smaller than the cross sectional area of said nozzle barrel at an end of said nozzle barrel.

Preferably, said initial atomization section comprises a length of feed pipe having an upstream end connective with a source of liquid feed, a downstream end with an unobstructed or open outlet and plurality of atomizing gas injection holes drilled through said feed pipe and radially distributed about said pipe and within one feed pipe diameter of said outlet, and an atomizing gas distribution section having an inlet for atomizing gas and an outlet encompassing said plurality of atomizing gas injection holes.

Desirably said impingement section comprises a cylindrical plug having an upstream end and a downstream end which is axially aligned with said initial atomization section. The upstream end of said plug preferably has a conical end portion with an angle no greater than 20°.

The plug can be supported at the downstream end thereof, and the support preferably comprises an X or cross-shaped support means, and wherein the support means has a cross sectional area, perpendicular to fluid flow, of 40 to 60 % of the area available for fluid flow immediately upstream of the support means, and said support means splits fluid flowing therethrough into several streams. The downstream support for the cylindrical plug is adapted to split the fluid flowing therethrough into four pie-shaped streams. An outlet of said annular expansion region may comprises said downstream support for said cylindrical plug.

The annular expansion region is desirably axially aligned with said nozzle barrel and has an outlet contiguous with said nozzle barrel. The annular expansion region preferably comprises a truncated conical section having an inlet contiguous with said atomization section, and the nozzle barrel is preferably cylindrical.

The nozzle outlet may comprises a dome or 180° hemi-spherical cap with a rectangular slot opening. Preferably the slot opening is less than 180° and produces a spray angle of 35 to 120°, more preferably 40 to 90°.

The annular expansion region may have a cross sectional area at least as large as the cross sectional area of said partially atomized jet and said expansion region connects with a nozzle barrel having a cross sectional area at least twice as large as said cross sectional area of said partially atomized jet.

In one construction the nozzle outlet comprises a slot or notch adapted to develop a flat, fan shaped spray, and said nozzle barrel has a length and a diameter, and the ratio of the length to diameter ranges from 3:1 to 15:1, preferably

from 3:1 to 6:1, and more preferably 4:1. The nozzle outlet ideally comprises a single rectangular notch outlet.

In said annular expansion region, the nozzle barrel preferably has a cross sectional area 1.5 to 6 times as large as the cross sectional area of said partially atomized jet, more preferably the nozzle barrel has a cross sectional area four times as large as the cross sectional area of said partially atomized jet.

According to another aspect of the invention there is provided a fluidized catalytic cracking process wherein a heavy feed is catalytically cracked in a riser cracking reactor means to produce cracked products and spent catalyst, spent catalyst is stripped in a stripping means and regenerated in a catalyst regeneration means to produce hot regenerated catalyst which is recycled to said riser reactor, wherein at least one multi-stage atomizing feed nozzle as described above is used to inject feed in a base portion of said riser reactor. Preferably a plurality of said nozzles are used. According to another aspect of the invention there is provided a process for adding a normally liquid hydrocarbon feed to a vapour/liquid fractionation means comprising adding said liquid feed and atomizing steam into a vapour phase region of said fractionation means using the nozzle described above.

According to another aspect of the invention there is provided a hydroconversion process for catalytic hydroconversion of a normally liquid hydrocarbon stream by adding hydrogen containing gas and liquid hydrocarbon to a vapour fill region above a fixed bed of catalyst and passing said liquid and hydrogen down through said fixed bed of catalyst at catalytic hydroconversion conditions to produce a hydroconverted product said normally liquid hydrocarbon feed, and at least a portion of said hydrogen containing gas, being added to said vapour full region above said fixed bed feed using the nozzle described above.

The nozzle according to the invention combines several different mechanisms for droplet formation, and achieves efficient atomization, with relatively low amounts of atomizing fluid, without requiring inordinately high oil feed pressures, or impinging on the wall of the riser reactor. The nozzle does not exhibit slugging characteristics, and can be mounted either vertically or at a slant, which permits its use in riser reactors having side mounted nozzles. The design is both robust and compact, and catalyst flows readily around it.

Reference is now made to the accompanying drawings, in which:

Fig 1 and Fig 2 (prior art) show different views of a 180° slotted cap nozzle outlet;

Figs. 3 and 4 show views of a shortened slot nozzle outlet;

Figure 5 shows a cross sectional view of a preferred nozzle according to the invention, with an initial atomizing section, low pressure drop plug and baffle (which also serves as an expansion section) and a shortened slot nozzle outlet;

Figures 6 and 7 show different views of the low pressure drop plug and baffle;

Figure 8 is a cross sectional view of the initial atomizing section;

Figure 9 is a cross sectional view of an FCC riser reactor with a plurality of feed nozzles; and

Figure 10 is a cross sectional view of the expansion plug, showing a preferred anchoring means.

The state of the art in regard to FCC feed nozzles, or at least feed nozzle outlets, is represented by Figs 1 and 2. The end of a nozzle 80', with notch or slot 85', sprays liquid feed into FCC risers. The feed upstream of the nozzle 80' is an atomized mixture of steam, or other atomizing fluid, and liquid hydrocarbon feed, usually with a minor amount of vaporized hydrocarbon feed. The slot orifice 85' is usually a cut out or ground out portion of the nozzle 80'. Typically the slot orifice has a 180° opening, and has a width or open portion equivalent to 15 - 50% of the diameter of the pipe or end cap 80' containing the slot orifice.

In these orifice nozzles, or those shown in the Oil and Gas Journal report referred to above, oil and steam are injected into a pipe, the end of which terminates in a reduced diameter orifice. The nozzle atomizes or disperses the oil by imparting a high velocity to the oil and atomizing steam. Poor results are obtained, especially with heavy, difficult to vaporize feeds. These nozzles were satisfactory when processing readily distillable feeds, such as gas oils, but their deficiencies become more evident with feeds containing more than about 5 wt % non-distillable material. The problem is that much of the liquid feed is poorly atomized. The large liquid droplets can take a long time to vaporize, or may not vaporize at all and form coke. In some units the feed is not vaporized until after the catalyst is significantly deactivated.

The FCC process and nozzle of the present invention use several mechanisms to form finely atomized droplets of heavy oil. An overview of the three atomization stages or mechanisms of a preferred nozzle follows, with primary reference to Fig 5, and passing reference to other Figs.

Briefly, the nozzle will have an initial atomization section, a low pressure drop impingement and expansion section, and an orifice tip.

The heavy oil or heavy liquid feed is charged via inlet 20 to atomizing chamber 22 of nozzle 10. Flange assembly 45 mates with flange 47 and nozzle shield 82 which extends into the FCC riser reactor.

The oil comes in inlet 20, usually as a liquid phase, and is atomized to a considerable extent as it flows through chamber 22 by the injection of steam transversely into the flowing liquid. Steam is admitted via atomizing fluid inlet 30. Flanges 35 and 25 around inlets 20 and 30, respectively, permit field connection of steam and oil lines.

The steam enters into the annular space 32 between the walls 34 of atomization chamber 22 and the walls 31 of nozzle 10. The steam passes through a plurality of holes 33 preferably drilled at right angles through pipe wall 34.

The heavy oil feed is vigorously mixed, and atomized to a significant extent, as it passes from inlet 20 to outlet 36 of the initial atomization zone. The liquid thus flows axially and the gas passes radially from the annular region 32 surrounding region 22.

Fig 8, which is a section of region 22 taken near the outlet end thereof, shows how steam can flow from the annular steam passageway 32 through holes 33 in pipe 34 to enter region 22 and atomize liquid feed flowing therethrough. Two rows of eight holes each are preferred.

Fig 5 shows the preferred arrangement of steam holes 33, within one or two pipe diameters upstream of the outlet 36 of this section. Preferably the steam holes are within 0.5 inch (1.3 cm) of the outlet 36. If desired, the steam injection holes 33 can be shifted upstream, or supplanted with additional steam injection means, such as slots, tubes, or minor amounts of steam added with the heavy oil feed.

The atomized two phase mixture from outlet 36 is discharged into a low pressure drop impingement and expansion section.

The first step is discharge of the oil/steam mixture directly onto impingement plug 50, which preferably has a cross sectional area no greater than that of the atomizing chamber 22. Ideally, the impingement plug 50 will have a cross sectional area from 30 to 60 % of the cross sectional area of the pipe 34. If pipe 34 is 1.5 inch (3.8cm) Schedule 80 pipe the optimum cross sectional area of plug 50 is around 1 inch (2.5cm). This is large enough to allow for impaction.

Plug 50 should be placed within a low pressure drop expansion region which permits efficient expansion of atomized oil and steam through this portion of the nozzle. The use of a truncated, inverted cone section 60 having an ID approaching or equalling that of the ID of the outlet of region 22 in pipe 34, and an angle of 5 to 30° from centerline, preferably 10 to 25°, and most preferably 15°, will minimize pressure losses due to expansion. More complex geometries, such as those used in venturi meters or carburetors may also be used, but such shapes are harder to fabricate and more expensive. Pin 50 may be somewhat displaced from, or recessed from, the outlet 36 of the initial atomization section, along the direction of liquid flow, by an amount equal to 0.5 inch (1.3cm) or more of the diameter of the outlet 36.

The angle of the inverted cone section 60, and the amount of recess of the impingement plug 50 from outlet 36, should be sufficient to provide a cross sectional area available for fluid flow around plug 50 at least equal to that of the cross sectional area available for fluid flow within pipe 34. Preferably the minimum open area of the pipe around the plug is at least 130 % or more of the cross sectional area of pipe 34. We believe the best spacing is one which will provide about 1.4 times the open area of the feed pipe 34.

Fig 7 shows a cross sectional view of a preferred impingement plug 50. The major purpose of plug 50 is as an impactor, upon which the atomized mixture of oil and steam strikes and further atomization occurs. Preferably the end of the plug is cut at a slight angle, ranging from 2 or 3° to perhaps as much as 15 or 20°, and ideally around 10°. This shallow angle allows for a strong impact of liquid and atomizing fluid against the plug and good atomization, while simultaneously channelling flow evenly around the plug and into the expansion section next to and downstream of the end of plug 50. The plug channels the atomized mixture away from the centre of the pipe into the expansion section.

The expansion section should have an outlet diameter roughly equal to that of the bore of the pipe or tube leading to the nozzle outlet. Preferably the expansion section terminates with a baffle section 65. Preferably the baffle is roughly in the form of a cross or "X", defining four pie shaped openings through which atomized feed passes. These baffles, shown as an interior view in Fig 6, preferably have a spoke width equal to 15 to 35 %, ideally 20 to 30 %, of the diameter of the outlet of the expansion section. A preferred design is the one shown, with a baffle plate having a thickness of 0.5 inch (1.3cm), and each spoke having a width of 0.69 inch (1.8cm), for use within a 3 inch (7.6cm) pipe.

This baffle design provides a good method of distributing droplets across the cross-section of the nozzle barrel, and provides enough metal or other material to support impingement plug 50. An alternative is to use a solid plate, with 2, 3, 4 or more holes drilled in the plate. Use of a solid plate with 4 holes drilled in it will behave hydraulically much like the "X" baffle shown by dotted lines in Fig. 6.

Regardless of the exact shape or configuration of the baffle 65, it is important to have sufficient open area so that there will be only a modest pressure drop across the baffle. Usually providing an open area of at least 25 % of the cross sectional area of the outlet of the expansion section will suffice.

Fig. 10 shows a preferred way of fabricating the plug and baffle assembly, relying on pin 67 to ensure proper

placement of the assembly in the nozzle. Field fabrication is greatly simplified, as the unit can not be installed backwards. Field replacement is also easy with such a design.

Baffles 65 promote further mixing of steam and oil, and ensure that the region of the nozzle downstream of the expansion section, and upstream of the nozzle outlet, i.e., the bore of the nozzle outlet, is loaded with an atomized mixture having a uniform droplet size and spray concentration. To this end, spiral mixers, swirl vanes, or baffle sections of varying geometry may be inserted at, or immediately upstream or downstream of the outlet of expansion section, but not necessarily with the same results.

There is a small pressure drop associated with the use of a plug, or plug and baffle, but this pressure drop is efficiently used by the system to atomize the mixture.

The method and apparatus of the present invention can use conventional orifice technology to discharge the atomized mixture into the riser reactor. In general, such orifices work best when the cross sectional area of the orifice is significantly less than the cross sectional area of the snout or barrel just upstream of the orifice. Broad variation in snout:slot areas is possible, but a 3.8:1 ratio gives good results.

The orifice may have additional atomizing means within or just downstream of the orifice tip, such as a spiral nozzle, but these generally will not be needed, and will increase the pressure drop, complexity, and failure rate unduly.

A slot orifice, in the form of a notch or slot 85 is shown in Fig 6. This forms a flat fan spray with an angle less than 180°. This is preferred for FCC use with side or circumferential mount nozzles. When nozzles are vertically mounted, a round orifice outlet is preferred.

The orifice may operate with wedge or deflector means or blocks just upstream of, within, or downstream of the orifice, if desired. These will increase the pressure drop through the nozzle, and the increased atomization efficiency will usually not justify the increased pressure drop. Swirl vanes seem to degrade performance. Thus it is preferred to operate with an orifice outlet consisting essentially of an orifice, preferably a slotted orifice defining a fan shaped spray.

The slotted orifice is preferred for side mounted nozzles, because experiments have shown that such a shape efficiently distributes the atomized mixture into the riser reactor. Although a prior art slot orifice, such as shown in Fig 1 or 2 can be used, it is preferred to use a slot which is shortened away from the tangent line of the cap, as shown in Fig 3 or 4. The slot orifice shown in Fig 3 and 4 will produce a spray angle of approximately 70-80°, which is a better spray angle for FCC than that produced by a slot orifice cut to the cup tangent line.

Use of such a reduced angle of spray allows the slotted orifice to be placed fairly near the walls of the riser reactor, without eroding the riser wall. Alternatively, the nozzle assembly can be inserted further into the riser reactor, with the increased distance from the riser wall providing some protection from wall erosion.

Fig 9 shows a good way to dispose FCC feed nozzles 10 in the base of an FCC riser reactor 1.

The effectiveness of the feed mixing nozzle of the present invention, was compared to several conventional designs, including an orifice tip nozzle, and an orifice tip nozzle having a spiral outlet.

The experiments were conducted with air/water mixtures, using a standard test procedure which had proved useful for predicting nozzle performance in FCC units. Although FCC units never inject water/air mixtures, by coincidence the flowing properties of these water/air mixtures are similar to those of steam/heavy oil mixtures used in FCC units.

The experiments were conducted in two stages - an initial screening test, followed by more rigorous tests.

The screening tests were run with nozzle exit velocities of 225 and 300 ft/s (69 and 91 m/s), and with dispersion air rates of 1.9 and 4.8 wt%, resulting in four combinations. Observations were qualitative - a video camera, with high shutter speed capability, was used to capture flow patterns and droplet sized more clearly. Tests were performed with the nozzles situated at 30° with respect to horizontal, to simulate the orientation of nozzles in many commercial FCC's with side mounted nozzles. Air was supplied at 100 psig (791KPa), using a large mobile compressor. Centrifugal pumps were used when high liquid flow rates or pressures were needed, with flow rates determined with a turbine or orifice flowmeter. The test procedure used is not critical, because the same test procedure was used for all nozzles.

Standard Commercial Nozzle - A nozzle currently used commercially in FCC units consists of a length of 3 inch (7.6cm) Schedule 40 pipe, with an oil inlet (water inlet) and steam (air) inlet in a "Y" inlet, so that the atomizing fluid was added at a slant, and in the direction of liquid flow. The two fluids flow together for about 3 ft (0.91m) before exiting through a cap with a semi-circular, rectangular slot, similar to that shown in Fig 1. Both atomization and droplet distribution were poor. Large droplets persisted in the centre and edge regions of the fan shaped, flat spray, while most of the air passed between these large droplet regions. Air and water pressure drops were relatively small. For this nozzle, and most of the others, spray became more uniform and less coarse for the test cases with higher exit velocities. Slugging within the two phase region of the 3 inch (7.6cm) cannon was noticed at the higher flow rates.

Spiral - A commercially available spiral nozzle was also tested. This was mounted on the 3 inch (7.6cm) cannon, with water and air premixed upstream. This nozzle operates by slicing off sheets from the inner cylindrical flow with a spiral cutting plane. This nozzle performed poorly at the 30° test angle since larger droplets predominated at the bottom, with finer droplets at the top. The distribution did improve substantially as the water flow rate increased, but the average droplet size also increased. This nozzle would be most effective when mounted nearly vertically. The air and water pressure drops were low to moderate. The spray contained gaps within the flow since the water remained predominantly

in the spiral sheet. The angle of the spray was also moderate, roughly 65°.

Lechler Supersonic - This nozzle has a converging section, with 16 air jets, emerging from 3/16 inch (0.48cm) orifices situated along four circumferential rows, which impinge perpendicularly into a cylindrical core of water. The nozzle then has a diverging section. This nozzle produced good atomization around the outer edge of the spray, but very large droplets persisted in the centre. It may be speculated that this might result from poor air jet penetration into the water, due to low jet velocities. The air jets created a back pressure affect which caused liquid pressure drops to be high for the standard conditions, 22-45 psi (152-310 KPa). Liquid pressure drops changed dramatically with air flow rates. Air pressure drops were low, ranging from 17-28 psi (117-193 KPa). The spray angle produced by the nozzle was very narrow.

SnowJet - This nozzle, manufactured by Spraying Systems Co. feeds air and water into a mixing chamber through fairly small orifices directed toward an impacting cylinder. A 2.5 ft (0.76m) snout, with semi-circular slot, was added by us on the end to create a spray pattern and exit velocity consistent with commercial FCCU requirements. This design achieved good atomization and droplet distribution, but at the cost of very high liquid pressure drop. When flow rates were low coarse droplets began to appear at the edges of the spray. Liquid pressure drops were high, ranging from 33 psi (228 KPa) up to 160 psi (1103 KPa) at the design point, while the air pressure drops were 20-55 psi (138-379 KPa). Two other caps were also tested, these were smaller ones used in snow making. They had smaller exit orifices, which increased pressure drop and exit velocity, but still achieved good atomization. These small exit orifice nozzles had too small a spray pattern, and too high an exit velocity to have much practical utility as FCC feed nozzles.

Modifications - Several modifications were made to some of the standard designs, some of which degraded performance, or resulted in unacceptable increases in pressure drop.

Adding swirl vanes upstream of the standard commercial nozzle discussed above produced a highly distorted "s" shaped spray, with coarse droplets at the edges.

When using a slot orifice outlet on a commercially available nozzle with internal swirl vanes, the swirling forced large droplets of water toward the edges, while the air bypassed through the middle.

Invention - Good atomization could be achieved using a nozzle with three sections or stages - an initial atomizing section, an impingement plug with low pressure drop expansion section, and an orifice outlet. All parts of the nozzle work together to achieve the desired result. Some conventional nozzle technology can be used in some parts of the nozzle, e.g., an initial atomizing section, or an orifice outlet, similar to that of some prior art nozzles, may be used, with some degradation in performance. Each section or stage will be reviewed in more detail below, along with some of the experimental work that went into devising each section.

Atomizing of feed is an essential first stage in the nozzle. The atomizing section bears some resemblance to the Lechler Supersonic nozzle, but it is not the same. The following differences can be noted. Our design does not require a gradually converging section, but can simply use a length of straight pipe. Rather than add atomizing vapour at four locations (four rings of holes), the atomizing vapour is added via just two locations (two rings). The air holes were sized to utilize fully the pressure drops available on the gas side.

The Leuchler Supersonic, and similar types of nozzles, work well around the edges, but have a core problem, that is large droplets tend to persist in the centre of the spray. Going to higher gas rates improves atomization, but can cause a dramatic change in liquid pressure drop.

The preferred design according to the invention, which uses two rows or rings of holes, makes excellent use of all the pressure energy available in the atomizing gas.

The injection of at least one stage of atomizing vapour into a core of liquid via a plurality of radially distributed orifices works well. One ring of four orifices, located within one pipe diameter of the outlet of this section, is probably the minimum configuration, but use of two rows, each with eight orifices is believed optimum.

The impingement plug, with low pressure drop expansion section, is an important part of the invention. At its simplest it need only consist of a single impingement plug having a cross-sectional area, as measured in the direction of flow ranging from 25 to 150 %, and preferably from 30 to 60 %, and most preferably about 40 to 55 % of the upstream section or feed pipe.

It is especially beneficial if the impingement plug has a cut or ground surface, deflecting flow around the impingement plug with a very shallow cut, not more than 20°, and preferably about 10°. The plug acts as an impactor, upon which the feed strikes and further atomization occurs. The shallow cut, at the end of the plug, channels flow evenly into an annular opening around the plug. Fig 7 shows a preferred impingement plug 50 with ground end.

The open area, or annular area around the plug should be at least as large as the open area of the feed pipe. The optimum open area, for the cut plug tested, is believed to be around 1.4 times the open area of the feed pipe. The relatively large open area, and the deflection action of the impingement pin, provide further atomization, especially of the large droplets that may remain in the central flow regions of the feed pipe. Preferably the annular area is defined at least in part by an expansion area, such as area 60, in which the nozzle ID makes the transition from the relatively narrow atomizing region 22 to the much larger region 62 upstream of the nozzle outlet.

Preferably there is a 5° to 30°, and most preferably a 10° to 20° angle, overall as measured from the centerline,

expansion area from the oil feed pipe to the large nozzle pipe. This shallow angle minimises pressure losses due to expansion, which allows available pressure to be used in atomization of feedstock, rather than simply lost due to passing through a sudden expansion of the pipe. The 15° shown in Fig 5 is believed optimum. Use of more exotic shapes, such as a venturi section, may further reduced pressure drop. The preferred plug design has such a low pressure drop associated with it that the higher cost of exotic shapes will not be worth the marginal reduction in pressure drop.

Preferably the expansion region ends with a baffle effective to promote some additional mixing and uniform distribution of droplets in the region upstream of the nozzle outlet. The preferred baffle is a cross shaped means which distributes flow evenly through four large pie-shaped orifices.

The nozzle according to the invention, like many nozzle designs of the prior art, works best with some type of orifice outlet. Although any of the conventional orifice outlets known in the art can be used (such as those shown in the Oil & Gas Journal Article previously discussed), the design works best with a slotted cap outlet such as that shown in Figs 3 and 4. A circular orifice can be used for vertically mounted nozzles, while slots developing a relatively wide fan shaped spray can be used for nozzles mounted circumferentially around the perimeter of an FCC riser.

For use in FCC, the slot open area should be sized to provide an exit velocity of 150 to 450 ft/s (46 to 137 m/s), preferably 200 to 350 ft/s (61 to 107 m/s), and most preferably around 300 ft/s (91 m/s). This is a moderately high exit velocity, which gives the nozzle spray sufficient energy to mix well with the hot catalyst, but not so high as to cause attrition of the catalyst nor carry across the catalyst and impinge on the opposite wall of the riser. Use of a notched or slot outlet, developing a flat, fan shaped spray, avoids formation of a concentrated stream of oil, which might penetrate across the riser.

In the preferred nozzle configuration, all parts function in a complementary fashion. The initial atomizing section does a good job of atomizing most of the liquid feed. The impingement plug does very little to the well atomized oil near the walls of the atomizing section, but is ideally placed to atomize the modest amount of larger droplets remaining in the central regions of the atomizing section, furthest from the wall. Mixing intensity decreases radially inward from the wall of the atomizing section, while the reverse is true in the plug section, where the mixing intensity is highest in the centre.

Additional mixing occurs as the well atomized mixture passes through the four pie shaped openings, and again when the mixture splits to some extent to get through the slot shaped nozzle outlet, which is preferably rotated 45° from the pie shaped openings.

When a notch shaped outlet, generating a flat, fan shaped spray, is used, there is a strong interaction between the baffle and the orifice, which even involves the length of the snout or nozzle barrel holding the orifice. The baffles just downstream of the impingement plug significantly improve performance when a slot outlet is used. There seems to be a significant degradation in performance, in forcing the atomized stream to shift from a generally circular distribution (around the impingement pin) to a flat fan shaped spray. Use of the baffles, and providing sufficient length of nozzle barrel upstream of the slot orifice to let the pie shaped sprays mix in the nozzle barrel, maintains good atomization. The optimum length of the snout, or length of pipe between the slot orifice and the baffles, is about 4 pipe diameters, but longer or shorter lengths have given acceptable results.

A series of qualitative (screening) and quantitative tests were conducted. A nozzle, very similar to that shown in Fig 5 was used for the tests. The basic nozzle design consisted of an atomizing section (two varieties were tested), an impingement plug with pie shaped opening baffle downstream of the plug, and a length of 3 inch (7.6cm) pipe with a cap with a horizontal slot at the end.

Two atomization sections were tested, one with eight, 5/32 inch (0.4cm) annular air orifices which impinged upon a core of water at 45°, within a region of expansion. This is not shown in the figs. The second, and preferred, design used sixteen, 1/8 inch (0.32cm) annular air orifices situated upstream of the expansion region.

The nozzles tested were oriented vertically downward, to accommodate the analyzing equipment. A droplet size analyser was used to digitise a black and white image of part of the spray which passes through a narrow gap in the line of sight of a video camera. A gap length of 13 mm was used for the experiments. The droplets were back illuminated by a strobing Xenon laser. To ensure statistical significance, data were acquired so that at least 10,000 droplets were analysed. To avoid including erroneously large drops, usually due to splattering, we excluded any single droplet that contributed to more than 10 % of the volume of all droplets. This rarely had to be done, though, since the possibility of this happening was reduced by counting large numbers of droplets during each test. Droplet sizes were calculated as the Sauter mean droplet size, defined as the diameter of a sphere which has the same volume/surface area ratio as that of the total droplet population. Relative droplet sizes were then calculated for each set of tests. Tests were run at various nozzle exit velocities, and with varying amounts of air.

Additional tests were then conducted to determine the effectiveness of the slotted orifice outlet. The same nozzle body was used, for all tests, with both types of atomization sections. In one set of tests, no impingement plug or cap was used. This produced a relatively narrow spray angle of 20° - 30°. In the other series of tests, the 0.8 x 2.9 inch (2 x 7.4cm) slot in a cap was affixed to the end of the nozzle. The tests are presented in two groupings in Tables I and II,

the first being with eight orifices discharging air into the expansion section, and the second being with sixteen orifices, as shown in Fig 5

A comparison of Tables I and II show that the sixteen orifice nozzle design produces a spray with a significantly smaller dropsizes than the eight orifice design. In the sixteen hole design the steam jets impinge upon the feed in a perpendicular direction, which provides for maximum utilisation of the available steam flowrate and pressure.

The impact of several key variables can also be analysed from the data in Table I. The effects of exit velocity and wt% steam are both significant to the performance of the nozzle. As the exit velocity increases at constant wt% steam, the atomization improves. This is also true of wt% steam, as the amount of steam increases relative to the amount of feed (at constant exit velocity), the atomization improves. From 300 to 225 ft/s (91 to 68 m/s) exit velocity and 5 to 2 wt% steam, the performance of the nozzle declines incrementally, but below those values, the decrease in performance becomes more rapid.

Table III studies the impact of the plug and baffle piece and the slotted cap on the atomization performance of the nozzle. Both the eight and sixteen steam orifice tables clearly indicate that the atomization improves with the addition of the plug and baffle and the slotted cap. Comparing the two nozzles, however, shows that the improvement gained by the addition of these pieces is much greater for the eight hole design. This is because the initial atomization generated by the sixteen hole design at the impingement point is very good; there is not as much room for further atomization downstream. The data show that the improvement caused by the plug and baffle and slotted cap for the eight hole design is 30-53%, while the improvement for the sixteen hole design is only 10-15%. What this means is that the sixteen holes do an excellent job of atomizing the feed, and that the plug and cap, while adding some atomization, are mainly responsible for the distribution and formation of the spray pattern.

These tests show that the nozzle according to the invention functions very well using a combination of initial atomization, impaction, and expansion. The nozzle should be widely applicable in refinery and petrochemical processes, and not subject to plugging. The only fine holes in the preferred design are used to admit high pressure steam to the initial atomizing section. The portions of the nozzle wet by hydrocarbon oil (or other liquid feed) are relatively open, i. e., the cross sectional area available for flow around the impingement plug 50 is larger than the cross sectional area available for fluid flow in the initial atomization section 22.

As applied to hydrotreaters, the use of such a nozzle will significantly improve catalyst use and minimize channelling of feed through the fixed bed of hydrotreating catalyst.

As applied to hydrocrackers, the use of our nozzle will greatly improve the efficiency and the safety of the process, by preventing liquid mal-distribution, which can lead to localised areas of high temperature which tend to travel through the hydrocracking bed and get worse. The nozzle can be used for adding liquid feed, and/or liquid quench to hydrocrackers.

The nozzle of the present invention may also be used to add any essentially solids free vapour/liquid phase to any refinery unit operation. The efficiency of packed towers will be greatly improved if the feed is added via an orifice tip nozzle with swirl vanes. In such an application the vapour present in the two phase feed will usually be sufficient to disperse the liquid over the packed column.

TABLE I
Extended Data for the New Nozzles
NEW NOZZLE DESIGN WITH 16 ORIFICES

Run Number	Air wt. %	Exit Velocity ft/s	Exit Velocity m/s	Exit Density lb/cu.ft	Exit Density $\text{gm}^3 \cdot 10^3$	Water Flow gpm	Water Flow ℓ/s	Air Flow scfm	Air Flow ℓ/s	Pressure Drop Liquid $\text{g/m}^2 \cdot 10^7$	Pressure Drop (psi) Gas $\text{g/m}^2 \cdot 10^7$	Relative Droplet size
1	1.0	150	45.7	6.89	110.4	118	7.4	129	60.9	29	30.0	3.40
2	1.0	225	68.6	6.89	110.4	177	11.2	194	91.6	56	57.8	3.58
3	1.0	300	91.5	6.89	110.4	235	14.8	259	122.2	87.6	90.5	2.78
4	2.0	150	45.7	3.68	58.9	62	3.9	137	64.7	15.5	16.0	3.13
5	2.0	225	68.6	3.68	58.9	93	5.9	205	96.7	31	32.0	1.65
6	2.0	300	91.5	3.68	58.9	124	7.8	273	128.9	47	48.6	1.11
7	5.0	150	45.7	1.57	25.1	26	1.6	142	67.0	6	6.2	2.60
8	5.0	225	68.6	1.57	25.1	39	2.5	212	100.1	13.1	13.5	1.44
9	5.0	300	91.5	1.57	25.1	52	3.3	283	133.6	22	2.7	1.00
10	5.0	350	106.7	1.57	25.1	60	3.8	330	155.8	29.1	30.1	1.40

TABLE II
ALTERNATE OZZLE DESIGN WITH 8 ORIFICES

Run Number	Air wt. %	Exit Velocity ft/s m/s	Exit Density lb/cu.ft $\text{gm}^3 \cdot 10^3$	Water Flow gpm ℓ/s	Air Flow scfm ℓ/s	Pressure Drop Liquid $\text{g/m}^2 \cdot 10^7$	(psi) Gas	$\text{g/m}^2 \cdot 10^7$	Relative Droplet size
1	2.0	150 45.7	3.68	62 3.9	137 64.7	7.5 7.7	37.5	38.7	3.22
2	2.0	225 68.6	3.68	93 5.9	205 96.7	18 18.6	57	58.9	1.71
3	2.0	300 91.5	3.68	124 7.8	273 128.9	28 28.9	88.8	91.9	1.22
4	5.0	150 45.7	1.57	26 1.6	142 67.0	2 2.1	36	37.2	3.21
5	5.0	225 68.6	1.57	39 2.5	212 100.1	7 7.2	61.5	63.5	1.66
6	5.0	300 91.5	1.57	52 3.3	283 133.6	13 13.4	90.8	93.8	1.27

TABLE III
Extended Data for the New Nozzles

NEW NOZZLE DESIGN

Spray Angle: 60°-80° (with Plug and Cap)
20°-30° (No Plug and Cap)

Exit size: 0.8" x 2.9"
2.0cm x 7.4cm

8 Steam Orifices

New Nozzle Design Options	Exit Velocity ft/sec	Exit Velocity m/s	Gas wt %	Pressure Drop Liquid	Pressure Drop Gas	Relative Droplet size
No Plug and Cap	225	68.6	2	4	4.1	62.7
w/Plug and Cap	225	68.6	2	18	18.6	57
No Plug and Cap	300	91.5	5	2	2.1	88
w/Plug and Cap	300	91.5	5	13	13.4	90.8
						96.9
						1.27

16 Steam Orifices

New Nozzle Design Options	Exit Velocity ft/sec	Exit Velocity m/s	Gas wt %	Pressure Drop Liquid	Pressure Drop Gas	Relative Droplet size
No Plug and Cap	225	68.6	2	25	25.8	55.5
w/Plug and Cap	225	68.6	2	31	32.0	57.5
No Plug and Cap	300	91.5	5	18	18.6	84.7
w/Plug and Cap	300	91.5	5	22	22.7	79.1
						81.7
						1.00

Claims

1. A fluidized catalytic cracking process wherein a heavy feed is catalytically cracked in a riser cracking reactor means to produce cracked products and spent catalyst, spent catalyst is stripped in a stripping means and regenerated in a catalyst regeneration means to produce hot regenerated catalyst Which is recycled to said riser reactor, wherein at least one multi-stage atomizing feed nozzle is used to inject feed in a base portion of said riser reactor, said nozzle comprising:

an initial atomization section wherein atomizing gas is charged, in radial out-to-in flow, into a flowing stream containing liquid hydrocarbon, to partially atomize said liquid feed stream and produce a partially atomized jet having a diameter and cross sectional area and having a less atomized core region and a more atomized

peripheral region;

an impingement section contiguous with and downstream of said initial atomization section, and having a diameter no greater than 150% of the diameter of said initial atomization section;

an annular expansion region about said impingement section, said expansion region having a cross sectional area at least as large as said partially atomized jet and connective with a nozzle barrel having a cross sectional area at least 1.5 times as large as the cross sectional area of said partially atomized jet; and

a nozzle outlet having a cross sectional area smaller than the cross sectional area of said nozzle barrel at an end of said nozzle barrel.

2. A process according to claim 1, wherein a plurality of said nozzles is used.
3. A process according to claim 1 or 2, wherein the impingement section is axially aligned with said initial atomisation section.
4. A process according to claim 1, 2, or 3, wherein said initial atomization section comprises a length of feed pipe having an upstream end connective with a source of liquid feed, a downstream end with an unobstructed or open outlet and plurality of atomizing gas injection holes drilled through said feed pipe and radially distributed about said pipe and within one feed pipe diameter of said outlet, and an atomizing gas distribution section having an inlet for atomizing gas and an outlet encompassing said plurality of atomizing gas injection holes.
5. A process according to any preceding claim, wherein said impingement section comprises a cylindrical plug having an upstream end and a downstream end which is axially aligned with said initial atomization section.
6. A process according to claim 5, wherein the upstream end of said plug has a conical end portion with an angle no greater than 20°.
7. A process according to claim 5 or 6, wherein the plug is supported at the downstream end thereof.
8. A process according to claim 7, wherein the downstream support comprises an X or cross-shaped support means, and wherein the support means has a cross sectional area, perpendicular to fluid flow, of 40 to 60 % of the area available for fluid flow immediately upstream of the support means, and said support means splits fluid flowing therethrough into several streams.
9. A process according to claim 8, wherein said downstream support for the cylindrical plug is adapted to split the fluid flowing therethrough into four pie-shaped streams.
10. A process according to any preceding claim, wherein the annular expansion region is axially aligned with said nozzle barrel and has an outlet contiguous with said nozzle barrel.
11. A process according to claim 10, wherein said outlet of said annular expansion region comprises said downstream support for said cylindrical plug.
12. A process according to claim 10 or 11, wherein the annular expansion region comprises a truncated conical section having an inlet contiguous with said atomization section.
13. A process according to any preceding claim, wherein said nozzle barrel is cylindrical.
14. A process according to any preceding claim, wherein said nozzle outlet comprises an orifice.
15. A process according to claim 14, wherein said nozzle outlet comprises a dome or 180° hemi-spherical cap with a rectangular slot opening.
16. A process according to claim 15, wherein the slot opening is less than 180° and produces a spray angle of 35 to 120°, preferably 40 to 90°.

17. A process according to any preceding claim, wherein said annular expansion region about said impingement section has a cross sectional area at least as large as the cross sectional area of said partially atomized jet and said expansion region connects with a nozzle barrel having a cross sectional area at least twice as large as said cross sectional area of said partially atomized jet.

18. A process according to any one of claims 1 to 13, wherein said nozzle outlet comprises a slot or notch adapted to develop a flat, fan shaped spray, and said nozzle barrel has a length and a diameter, and the ratio of the length of diameter ranges from 3:1 to 15:1.

19. A process according to claim 18, wherein said nozzle barrel has a length to diameter ratio of from 3:1 to 6:1, preferably 4:1.

20. A process according to claim 17, 18 or 19 wherein said nozzle outlet comprises a single rectangular notch outlet.

21. A process according to any preceding claim, wherein, in said annular expansion region, the nozzle barrel has a cross sectional area 1.5 to 6 times as large as the cross sectional area of said partially atomized jet.

22. A process according to claim 21, wherein, in said annular expansion region, the nozzle barrel has a cross section area four times as large as the cross sectional area of said partially atomized jet.

23. An atomizing nozzle comprising:

an initial atomization section wherein atomizing gas is charged, in radial out-to-in flow, into a flowing stream containing liquid hydrocarbon, to partially atomize said liquid feed stream and produce a partially atomized jet having a diameter and cross sectional area and having a less atomized core region and a more atomized peripheral region;

an impingement section contiguous with a downstream of said initial atomization section, and having a diameter no greater than 150% of the diameter of said initial atomization section;

an annular expansion region about said impingement section, said expansion region having a cross sectional area at least as large as said partially atomized jet and connective with a nozzle barrel having a cross sectional area at least 1.5 times as large as the cross sectional area of said partially atomized jet; and

a nozzle outlet having a cross sectional area smaller than the cross sectional area of said nozzle barrel at an end of said nozzle barrel.

24. A nozzle according to claim 23, wherein the diameter of the cylindrical nozzle is at least twice as large as the diameter of said initial atomizer.

25. A process for adding a normally liquid hydrocarbon feed to a vapour/liquid fractionation means comprising adding said liquid feed and atomizing steam into a vapour phase region of said fractionation means using the nozzle of claim 23 or 24.

26. A hydroconversion process for catalytic hydroconversion of a normally liquid hydrocarbon stream by adding hydrogen containing gas and liquid hydrocarbon to a vapour fill region above a fixed bed of catalyst and passing said liquid and hydrogen down through said fixed bed of catalyst at catalytic hydroconversion conditions to produce a hydroconverted product characterized by adding said normally liquid hydrocarbon feed to and at least a portion of said hydrogen containing gas to said vapour full region above said fixed bed feed using the nozzle of claim 23 or 24.

Patentansprüche

1. Verfahren zum katalytischen Cracken in der Wirbelschicht, bei dem man einen schweren Einsatzstoff in einem Riser-Crackreaktor katalytisch crackt, wobei man Crackprodukte und verbrauchten Katalysator erhält, den verbrauchten Katalysator in einem Abstreifer abstreift und in einem Katalysator-Regenerator regeneriert, wobei man heißen regenerierten Katalysator erhält, den man in den Riser-Reaktor zurückführt, wobei man zur Einspritzung von Einsatzstoff in einen Bodenteil des Riser-Reaktors mindestens eine mehrstufige Einsatzstoff-Zerstäuberdüse verwendet, welche enthält:

einen am Anfang angeordneten Zerstäubungsabschnitt, in dem Zerstäubungsgas in von außen nach innen gerichtetem Radialstrom einem flüssigen Kohlenwasserstoff enthaltenden fließenden Strom zugeführt wird, wodurch der flüssige Einsatzstrom teilweise zerstäubt wird und ein teilzerstäubter Strahl mit einem Durchmesser und einer Querschnittsfläche sowie einem weniger zerstäubten Kernbereich und einem mehr zerstäubten Randbereich entsteht;

einem an den am Anfang angeordneten Zerstäubungsabschnitt angrenzenden und stromabwärts gelegenen Aufprallbereich mit einem Durchmesser, der nicht größer als 150% des Durchmessers des am Anfang angeordneten Zerstäubungsabschnitts ist;

einem um den Aufprallbereich angeordneten ringförmigen Ausdehnungsbereich mit einer Querschnittsfläche, die mindestens so groß wie der teilzerstäubte Strahl ist und mit einem Düsenlauf mit einer Querschnittsfläche, die mindestens 1,5mal so groß wie die Querschnittsfläche des teilzerstäubten Strahls ist, verbunden ist; und einem Düsenausgang mit einer Querschnittsfläche, die kleiner als die Querschnittsfläche des Düsenlaufs an einem Ende des Düsenlaufs ist.

2. Verfahren nach Anspruch 1, bei dem man mehrere der Düsen einsetzt.
3. Verfahren nach Anspruch 1 oder 2, wobei der Aufprallabschnitt mit dem am Anfang angeordneten Zerstäubungsabschnitt axial in einer Linie angeordnet ist.
4. Verfahren nach Anspruch 1, 2 oder 3, wobei der am Anfang angeordnete Zerstäubungsabschnitt aus einem Speiserohr mit einem mit einer Quelle des flüssigen Einsatzstoffs verbundenen stromaufwärts gelegenen Ende, einem stromabwärts gelegenen Ende mit einem unversperrten oder offenen Auslaß und mehreren durch das Speiserohr gebohrten, radial um das Rohr verteilten und innerhalb eines Speiserohr-Durchmessers des Auslasses gelegene Zerstäubungsgas-Einspritzlöchern und einem Zerstäubungsgas-Verteilungsabschnitt mit einem Einlaß für Zerstäubungsgas und einem die mehreren Zerstäubungsgas-Einspritzlöcher umfassenden Auslaß.
5. Verfahren nach einem der vorhergehenden Ansprüche, wobei der Aufprallabschnitt aus einem zylindrischen Kolben mit einem stromaufwärts gelegenen Ende und einem mit dem am Anfang angeordneten Zerstäubungsabschnitt axial in einer Linie angeordneten stromabwärts gelegenen Ende.
6. Verfahren nach Anspruch 5, wobei das stromaufwärts gelegene Ende des Kolbens einen kegelförmigen Endteil mit einem Winkel von höchstens 20° aufweist.
7. Verfahren nach Anspruch 5 oder 6, wobei der Kolben an seinem stromabwärts gelegenen Ende befestigt ist.
8. Verfahren nach Anspruch 7, wobei die stromabwärts gelegene Halterung X- oder kreuzförmig ist, senkrecht zum Fluidstrom eine Querschnittsfläche von 40 bis 60% der unmittelbar stromaufwärts des Trägers für Fluidstrom zur Verfügung stehenden Fläche aufweist und durch sie strömendes Fluid in mehrere Ströme zerteilt.
9. Verfahren nach Anspruch 8, wobei die stromabwärts gelegene Halterung für den zylindrischen Kolben zur Zerteilung des durch sie strömenden Fluids in vier tortenstückförmige Ströme ausgelegt ist.
10. Verfahren nach einem der vorhergehenden Ansprüche, wobei der ringförmige Ausdehnungsabschnitt mit dem Düsenlauf axial in einer Linie angeordnet ist und einen an den Düsenlauf angrenzenden Auslaß aufweist.
11. Verfahren nach Anspruch 10, wobei der Auslaß des ringförmigen Ausdehnungsabschnitts die stromabwärts gelegene Halterung für den zylindrischen Kolben enthält.
12. Verfahren nach Anspruch 10 oder 11, wobei der ringförmige Ausdehnungsabschnitt einen kegelstumpfförmigen Abschnitt mit einem an den Zerstäubungsabschnitt angrenzenden Einlaß enthält.
13. Verfahren nach einem der vorhergehenden Ansprüche, wobei der Düsenlauf zylindrisch ist.
14. Verfahren nach einem der vorhergehenden Ansprüche, wobei der Düsenausgang eine Austrittsöffnung darstellt.
15. Verfahren nach Anspruch 14, wobei der Düsenausgang eine Kuppel oder eine 180° umspannende halbkreisförmige Abdeckung mit einem rechteckigen Schlitz enthält.

16. Verfahren nach Anspruch 15, wobei der Schlitz zu weniger als 180° offen ist und einen Sprühwinkel von 35 bis 120°, bevorzugt 40 bis 90°, erzeugt.
- 5 17. Verfahren nach einem der vorhergehenden Ansprüche, wobei der um den Aufprallbereich angeordnete ringförmige Ausdehnungsabschnitt eine Querschnittsfläche aufweist, die mindestens so groß wie die Querschnittsfläche des teilzerstäubten Strahls ist, und der Ausdehnungsbereich mit einem Düsenlauf mit einer Querschnittsfläche, die mindestens zweimal so groß wie die Querschnittsfläche des teilzerstäubten Strahls ist, verbunden ist.
- 10 18. Verfahren nach einem der Ansprüche 1 bis 13, wobei der Düsenausgang einen Schlitz oder eine Scharte enthält, der bzw. die zur Entwicklung eines flachen, fächerförmigen Sprays ausgelegt ist, der Düsenlauf eine Länge und einen Durchmesser aufweist und das Verhältnis von Länge zu Durchmesser im Bereich von 3:1 bis 15:1 liegt.
- 15 19. Verfahren nach Anspruch 18, wobei der Düsenlauf ein Verhältnis von Länge zu Durchmesser von 3:1 bis 6:1, bevorzugt 4:1, aufweist.
- 20 20. Verfahren nach Anspruch 17, 18 oder 19, wobei der Düsenausgang einen einzelnen rechteckigen schartenförmigen Auslaß darstellt.
21. Verfahren nach einem der vorhergehenden Ansprüche, wobei der Düsenlauf im ringförmigen Ausdehnungsabschnitt eine Querschnittsfläche aufweist, die 1,5- bis 6mal so groß wie die Querschnittsfläche des teilzerstäubten Strahls ist.
- 25 22. Verfahren nach Anspruch 21, wobei der Düsenlauf im ringförmigen Ausdehnungsabschnitt eine Querschnittsfläche aufweist, die viermal so groß wie die Querschnittsfläche des teilzerstäubten Strahls ist.
23. Zerstäuberdüse, enthaltend:
- einen am Anfang angeordneten Zerstäubungsabschnitt, in dem Zerstäubungsgas in von außen nach innen gerichtetem Radialstrom einem flüssigen Kohlenwasserstoff enthaltenden fließenden Strom zugeführt wird, wodurch der flüssige Einsatzstrom teilweise zerstäubt wird und ein teilzerstäubter Strahl mit einem Durchmesser und einer Querschnittsfläche sowie einem weniger zerstäubten Kernbereich und einem mehr zerstäubten Randbereich entsteht;
- 30 einem an den am Anfang angeordneten Zerstäubungsabschnitt angrenzenden und stromabwärts gelegenen Aufprallbereich mit einem Durchmesser, der nicht größer als 150% des Durchmessers des am Anfang angeordneten Zerstäubungsabschnitts ist;
- 35 einem um den Aufprallbereich angeordneten ringförmigen Ausdehnungsbereich mit einer Querschnittsfläche, die mindestens so groß wie der teilzerstäubte Strahl ist und mit einem Düsenlauf mit einer Querschnittsfläche, die mindestens 1,5mal so groß wie die Querschnittsfläche des teilzerstäubten Strahls ist, verbunden ist; und
- 40 einem Düsenausgang mit einer Querschnittsfläche, die kleiner als die Querschnittsfläche des Düsenlaufs an einem Ende des Düsenlaufs ist.
24. Düse nach Anspruch 23, wobei der Durchmesser der zylindrischen Düse mindestens doppelt so groß wie der Durchmesser des am Anfang angeordneten Zerstäubers ist.
- 45 25. Verfahren zum Zusatz eines normalerweise flüssigen Kohlenwasserstoff-Einsatzstoffs zu einer Dampf-Flüssigkeits-Fraktioniereinrichtung, bei dem man den flüssigen Einsatzstoff und den Zerstäubungsdampf mit der Düse nach Anspruch 23 oder 24 einem Gasphasenbereich der Fraktioniereinrichtung zuführt.
- 50 26. Hydrokonversionsverfahren zur katalytischen Hydrokonversion eines normalerweise flüssigen Kohlenwasserstoffstroms durch Zufuhr von wasserstoffhaltigem Gas und flüssigem Kohlenwasserstoff zu einem Dampf-Flüssigkeits-Fraktioniereinrichtung, bei dem man den flüssigen Kohlenwasserstoff-Einsatzstoff und den Zerstäubungsdampf mit der Düse nach Anspruch 23 oder 24 einem Gasphasenbereich der Fraktioniereinrichtung zuführt.
- 55

Revendications

1. Procédé de craquage catalytique fluidisé dans lequel une charge lourde est craquée catalytiquement dans un moyen avec réacteur de craquage à colonne montante pour produire des produits craqués et du catalyseur usé, le catalyseur usé est épuré dans un moyen d'épuration et régénéré dans un moyen de régénération de catalyseur pour produire du catalyseur régénéré chaud qui est recyclé vers ledit réacteur à colonne montante, dans lequel au moins un injecteur d'atomisation de charge à plusieurs étages est utilisé pour injecter la charge dans une partie de base dudit réacteur à colonne montante, ledit injecteur comprenant :
 - une section d'atomisation initiale dans laquelle du gaz d'atomisation est chargé, en un écoulement radial du dehors vers l'intérieur, dans un courant en écoulement contenant de l'hydrocarbure liquide, afin d'atomiser partiellement ce courant de charge liquide et de produire un jet partiellement atomisé ayant un diamètre et une aire de section transversale et comprenant une région centrale moins atomisée et une région périphérique plus atomisée;
 - une section d'impact contiguë à ladite section d'atomisation initiale et en aval de celle-ci, et ayant un diamètre non supérieur à 150% du diamètre de ladite section d'atomisation initiale;
 - une région de détente annulaire autour de ladite section d'impact, ladite région de détente ayant une aire de section transversale au moins aussi grande que ledit jet partiellement atomisé et en communication avec un fût d'injecteur ayant une aire de section transversale au moins 1,5 fois aussi grande que l'aire de section transversale dudit jet partiellement atomisé; et
 - une sortie d'atomiseur ayant une aire de section transversale plus petite que l'aire de section transversale dudit fût d'injecteur à une extrémité dudit fût d'injecteur.
2. Procédé suivant la revendication 1, dans lequel il est fait usage d'une pluralité desdits injecteurs.
3. Procédé suivant la revendication 1 ou 2, dans lequel la section d'impact est axialement alignée avec la section d'atomisation initiale.
4. Procédé suivant la revendication 1, 2 ou 3, dans lequel ladite section d'atomisation initiale comprend une longueur de tube de charge ayant une extrémité d'amont en communication avec une source de charge liquide, une extrémité d'aval présentant une sortie non obstruée ou ouverte et une pluralité de trous d'injection de gaz d'atomisation forés dans ledit tube de charge et répartis radialement autour dudit tube et dans les limites d'un diamètre de tube de charge de ladite sortie, et une section de distribution de gaz d'atomisation comprenant une entrée pour le gaz d'atomisation et une sortie embrassant ladite pluralité de trous d'injection de gaz d'atomisation.
5. Procédé suivant l'une quelconque des revendications précédentes, dans lequel ladite section d'impact comprend un tampon cylindrique comportant une extrémité d'amont et une extrémité d'aval qui est axialement aligné, avec ladite section d'atomisation initiale.
6. Procédé suivant la revendication 5, dans lequel l'extrémité d'amont dudit tampon comprend une partie d'extrémité conique avec un angle non supérieur à 20°.
7. Procédé suivant la revendication 5 ou 6, dans lequel le tampon est supporté à son extrémité d'aval.
8. Procédé suivant la revendication 7, dans lequel le support d'aval comprend un moyen de support en X ou forme de croix et dans lequel le moyen de support a une aire en section transversale, perpendiculaire à l'écoulement de fluide, de 40 à 60% de l'aire disponible pour l'écoulement de fluide immédiatement en amont du moyen de support et ledit moyen de support divise en plusieurs courants le fluide qui le traverse.
9. Procédé suivant la revendication 8, dans lequel le support en aval pour le tampon cylindrique est à même de diviser en quatre courants en forme de quart de cercle, le fluide qui le traverse.
10. Procédé suivant l'une quelconque des revendications précédentes, dans lequel la région de détente annulaire est axialement alignée avec ledit fût d'injecteur et comprend une sortie contiguë audit fût d'injecteur.
11. Procédé suivant la revendication 10, dans lequel ladite sortie de ladite région de détente annulaire comprend ledit support en aval pour ledit tampon cylindrique.

12. Procédé suivant la revendication 10 ou 11, dans lequel la région de détente annulaire comprend une section conique tronquée comportant une entrée contiguë à ladite section d'atomisation.
13. Procédé suivant l'une quelconque des revendications précédentes, dans lequel ledit fût d'injecteur est cylindrique.
14. Procédé suivant l'une quelconque des revendications précédentes, dans lequel ladite sortie d'injecteur comprend un orifice.
15. Procédé suivant la revendication 14, dans lequel ladite sortie d'injecteur comprend un dôme ou une calotte hémisphérique à 180° avec une ouverture en forme de fente rectangulaire.
16. Procédé suivant la revendication 15, dans lequel l'ouverture en forme de fente est de moins de 180° et produit un angle de pulvérisation de 35 à 120°, de préférence de 40 à 90°.
17. Procédé suivant l'une quelconque des revendications précédentes, dans lequel ladite région de détente annulaire autour de ladite section d'impact a une aire de section transversale au moins aussi grande que l'aire de section transversale dudit jet partiellement atomisé et ladite région de détente est en communication avec un fût d'injecteur ayant une aire de section transversale au moins deux fois aussi grande que ladite aire de section transversale dudit jet partiellement atomisé.
18. Procédé suivant l'une quelconque des revendications 1 à 13, dans lequel ladite sortie d'injecteur comprend une fente ou entaille propre à développer un jet plat en forme d'éventail et ledit fût d'injecteur a une longueur et un diamètre et le rapport de la longueur au diamètre s'échelonne de 3:1 à 15:1.
19. Procédé suivant la revendication 18 dans lequel ledit fût d'injecteur a un rapport de la longueur au diamètre de 3:1 à 6:1, de préférence de 4:1.
20. Procédé suivant la revendication 17, 18 ou 19, dans lequel ladite sortie d'injecteur comprend une sortie en entaille rectangulaire unique.
21. Procédé suivant l'une quelconque des revendications précédentes, dans lequel, dans ladite région de détente annulaire, le fût d'injecteur a une aire de section transversale 1,5 à 6 fois aussi grande que l'aire de section transversale dudit jet partiellement atomisé.
22. Procédé suivant la revendication 21, dans lequel, dans ladite région de détente annulaire, le fût d'injecteur a une aire de section transversale 4 fois aussi grande que l'aire de section transversale dudit jet partiellement atomisé.
23. Injecteur d'atomisation comprenant :
 - une section d'atomisation initiale dans laquelle du gaz d'atomisation est chargé, en écoulement radial du dehors vers l'intérieur, dans un courant en écoulement contenant de l'hydrocarbure liquide, afin d'atomiser partiellement ce courant de charge liquide et de produire un jet partiellement atomisé ayant un diamètre et une aire de section transversale et comprenant une région centrale moins atomisée et une région périphérique plus atomisée;
 - une section d'impact contiguë à ladite section d'atomisation initiale et en aval de celle-ci, et ayant un diamètre non supérieur à 150% du diamètre de ladite section d'atomisation initiale;
 - une région de détente annulaire autour de ladite section d'impact, ladite région de détente ayant une aire de section transversale au moins aussi grande que ledit jet partiellement atomisé et en communication avec un fût d'injecteur ayant une aire de section transversale au moins 1,5 fois aussi grande que l'aire de section transversale dudit jet partiellement atomisé; et
 - une sortie d'atomiseur ayant une aire de section transversale plus petite que l'aire de section transversale dudit fût d'injecteur à une extrémité dudit fût d'injecteur.
24. Injecteur suivant la revendication 23, dans lequel le diamètre de l'injecteur cylindrique est au moins deux fois aussi grand que le diamètre dudit atomiseur initial.
25. Procédé pour introduire une charge d'hydrocarbure normalement liquide dans un moyen de fractionnement vapeur/liquide, comprenant l'introduction de ladite charge liquide et de vapeur d'eau d'atomisation dans une région de

phase vapeur dudit moyen de fractionnement à l'aide de l'injecteur suivant la revendication 23 ou 24.

26. Procédé d'hydroconversion pour l'hydroconversion catalytique d'un courant d'hydrocarbure normalement liquide par introduction d'un gaz comprenant de l'hydrogène et de l'hydrocarbure liquide dans une région à remplissage de vapeur au-dessus d'un lit fixe de catalyseur et le passage du liquide et de l'hydrogène en sens descendant à travers ce lit fixe de catalyseur dans les conditions d'hydroconversion catalytique pour produire un produit hydro-converti, caractérisé par l'introduction de ladite charge d'hydrocarbure normalement liquide et d'au moins une partie dudit gaz contenant de l'hydrogène dans la région à remplissage de vapeur au-dessus dudit lit fixe à l'aide de l'injecteur suivant la revendication 23 ou 24.

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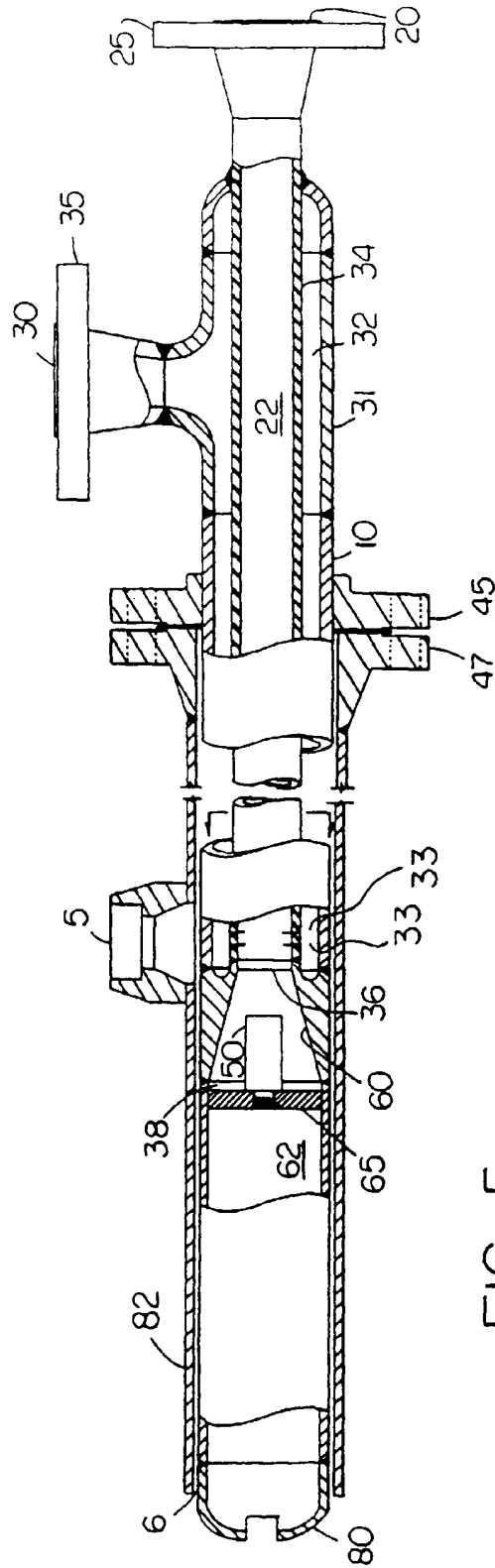
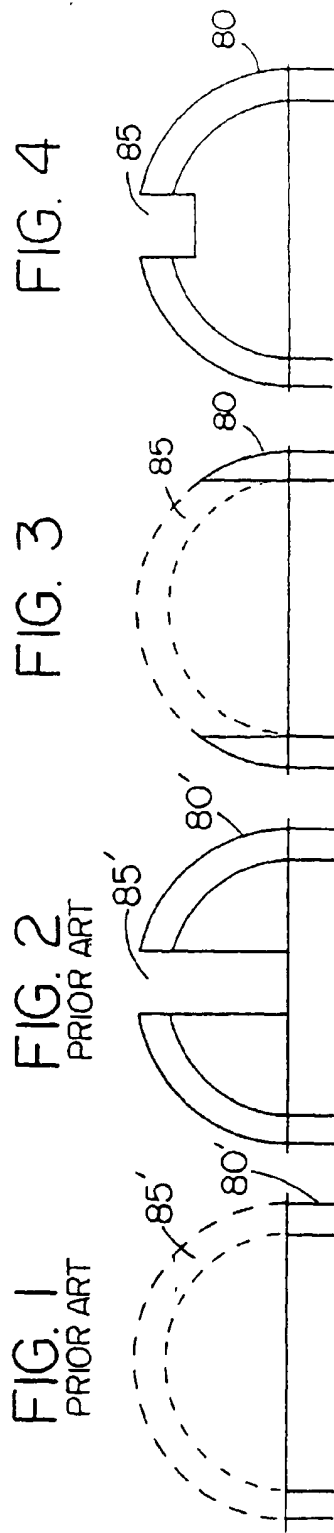


FIG. 5

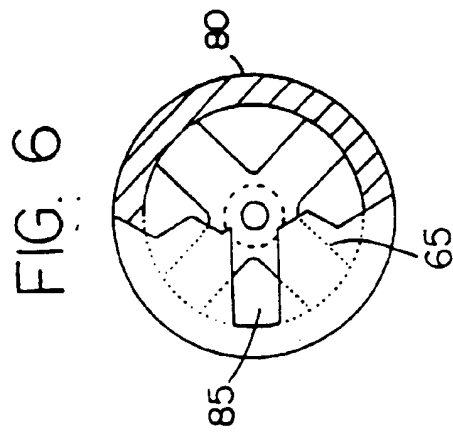
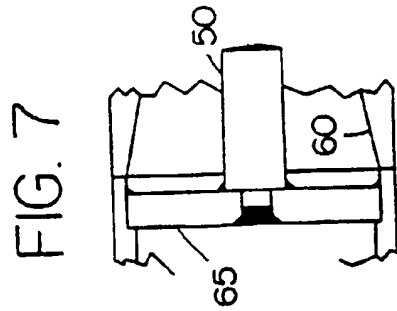
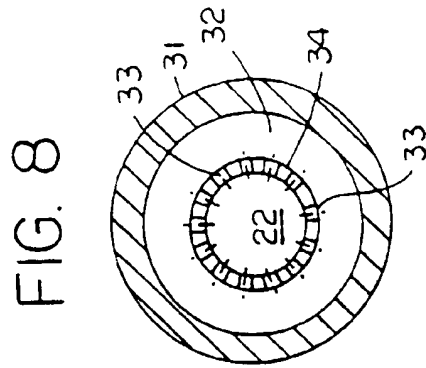


FIG. 10

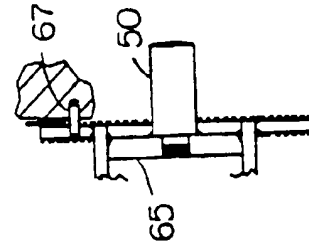


FIG. 9

